

**FREE CYLINDRICAL COUETTE FLOW OF A RAREFIED GAS WITH HEAT
TRANSFER, POROUS SURFACES AND ARBITRARY REFLECTION COEFFICIENT.**

M.A. KHIDR

Department of Math., Faculty of Science, Ain-Shams
University, Cairo, Egypt.

A.M. ABOURABIA

Department of Math., Faculty of Science, Menoufia
University, Shebin El-Kom Egypt.

M.A. MAHMOUD

Department of Math., Faculty of Science, Zagazig
University at Banha, Egypt.

ABSTRACT

Six nonlinear moments equations are used to replace the Boltzman equation describing the free flow of a rarefied gas between two fixed coaxial cylinders. The moments equations with the convenient boundary conditions-concerning heat transfer, porosity and reflection at the surfaces-are solved using small parameters method. The behaviour of the velocity, the density and the temperature is discussed.

I- INTRODUCTION:

The motion of a rarefied gas between two coaxial cylinders one fixed and the other rotates with constant angular velocity was studied by Galkin (1965) using the moments method for obtaining suitable solution for any Knudsen number. The heat transfer from a rarefied electron gas between two coaxial cylinders was investigated by Khidr and Abader (1976) this study revealed that, as the distance between the two cylinders decreases the rarefaction becomes more apparent, and at any degree of rarefaction there exists a minimum value for the density between the two cylinders. Abdel-Gaid and Khidr (1979) studied the problem of flow over a right circular cylinder-within the framework of the kinetic theory of gases-under constant electric field in the radial direction. The moments equations were solved by the small parameter method. The obtained solution showed that the behaviour of flow speed depends on those forces at infinity and was ineffective near the cylinder. Hady (1976) studied the motion of a rarefied gas between two coaxial circular porous cylinders, the inner is fixed while the outer is rotating with constant angular velocity, and the gas is of arbitrary degree of rarefaction. He considered the case, when the temperature difference between the two cylinders was small and the normal velocity to the porous surface was equal to a constant value.

In the present paper we consider the motion of a rarefied gas between two coaxial circular porous cylinders, the inner and the outer are fixed. The density and temperature are assumed to vary as the distance varies from the axis.

We adopt the case when the temperature difference between the cylinders is small and the accommodation coefficient ϵ is arbitrary.

II- THEORETICAL PREDICTIONS:

Considering a steady situation and free molecular flow, then the distribution function may be obtained from Boltzmann equation in cylindrical coordinates.

Free cylindrical Couette flow of a rarefied GAS with heat..

$$C_r \frac{\partial f}{\partial r} + C_\theta \left(\frac{1}{r} \frac{\partial f}{\partial \theta} \right) + C_z \frac{\partial f}{\partial z} = 0, \quad [1]$$

where, $f = f(\vec{r}, \vec{C})$ is the distribution function.

It is assumed that the distribution function of the molecules reflected from any surface with Maxwellian distribution differs from the density, velocity and temperature of that surface.

Multiplying equation [1] by any arbitrary function $\phi_i = \phi_i(\vec{C})$ we get:

$$\frac{d}{dr} \left[r \int \phi_i C_r f d\vec{C} \right] - \int C_\theta^2 f \frac{\partial \phi_i}{\partial C_\theta} d\vec{C} + \int C_r C_\theta f \frac{\partial \phi_i}{\partial C_\theta} d\vec{C} = 0, \quad [2]$$

where $C_r = C_n \sin \psi$, $C_\theta = C_n \cos \psi$.

For any quantity ϕ_i we have

$$\phi_i = \int_{\alpha=0}^{\pi-\alpha} \int_{-\infty}^{\infty} \phi_i f_1 d\vec{C} + \int_{\psi=\pi-\alpha}^{2\pi+\alpha} \int_{-\infty}^{\infty} \phi_i f_2 C_n dC_n dC_z d\psi, \quad [3]$$

where,

$$f_1 = \frac{n_1}{(2\pi RT_1)^{3/2}} \left(1 + \frac{V_1}{RT_1} C_r \right) e^{-C^2/2RT_1}; \quad \alpha < \psi < \pi - \alpha, \quad [4]$$

$$f_2 = \frac{n_2}{(2\pi RT_2)^{3/2}} \left(1 + \frac{V_2}{RT_2} C_r \right) e^{-C^2/2RT_2}; \quad \pi - \alpha < \psi < 2\pi + \alpha,$$

$$\cos \alpha = R_1/r.$$

V_1 and V_2 are the suction velocities out of the cylinders.

The six unknowns n_1, n_2, T_1, T_2, V_1 and V_2 are considered functions of the radial distance.

Hence, we have

$$n = \int f d\vec{C} = \frac{1}{2\pi} \left[(\pi - 2\alpha)n_1 + (\pi + 2\alpha)n_2 \right] + \frac{\cos \alpha}{\sqrt{4\pi R}} \left[\frac{n_1 V_1}{\sqrt{T_1}} - \frac{n_2 V_2}{\sqrt{T_2}} \right],$$

Khidr, Abourabia & Mahmoud.

$$\begin{aligned}
 V_r &= \frac{1}{n} \int C_r f dC \\
 &= \frac{1}{n} \left\{ \sqrt{\frac{R}{2\pi}} \cos \alpha (n_1 \sqrt{T_1} - n_2 \sqrt{T_2}) + \right. \\
 &\quad \left. + \frac{1}{2\pi} [(\pi - 2\alpha + \sin 2\alpha) n_1 V_1 + (\pi + 2\alpha - \sin 2\alpha) n_2 V_2] \right\}, \\
 T &= \frac{1}{n} \left\{ \frac{R}{2\pi} [(\pi - 2\alpha + \sin 2\alpha) n_1 T_1 + (\pi + 2\alpha - \sin 2\alpha) n_2 T_2] + \right. \\
 &\quad \left. + \sqrt{\frac{R}{2\pi}} (3 \cos \alpha - \cos^3 \alpha) (n_1 V_1 \sqrt{T_1} - n_2 V_2 \sqrt{T_2}) \right\}.
 \end{aligned}$$

where, n is the density, V_r is the mean velocity and T is the temperature.

For ϕ_i takes the values $1, C_r, C^2, C_r^2, C_\theta^2$ and $C_r C_\theta^2$ equation [2] gives:

$$\begin{aligned}
 [n_1 T_1^{3/2} - n_2 T_2^{3/2}] \cos \alpha + \frac{1}{\sqrt{2\pi R}} \{ (\pi - 2\alpha + \sin 2\alpha) n_1 V_1 + (\pi + 2\alpha - \sin 2\alpha) n_2 V_2 \} \\
 = \gamma_1 / r, \quad [5]
 \end{aligned}$$

where, γ_1 is arbitrary,

$$\begin{aligned}
 \frac{d}{dr} \{ [(\pi - 2\alpha + \sin 2\alpha) n_1 T_1 + (\pi + 2\alpha - \sin 2\alpha) n_2 T_2] + \\
 + \sqrt{\frac{2\pi}{R}} [(3 \cos \alpha - \cos^3 \alpha) (n_1 V_1 T_1^{1/2} - n_2 V_2 T_2^{1/2})] \} + \frac{4 \sin 2\alpha}{r} [n_1 T_1 - n_2 T_2] + \\
 + \frac{1}{r} \sqrt{\frac{2\pi R}{R}} [(3 \cos \alpha - 2 \cos^3 \alpha) (n_1 V_1 T_1^{1/2} - n_2 V_2 T_2^{1/2})] = 0, \quad [6]
 \end{aligned}$$

$$\begin{aligned}
 [n_1 T_1^{3/2} - n_2 T_2^{3/2}] \cos \alpha + \frac{5}{4 \sqrt{2\pi R}} \{ (\pi - 2\alpha + \sin 2\alpha) n_1 V_1 T_1 + \\
 + (\pi + 2\alpha - \sin 2\alpha) n_2 V_2 T_2 \} = \gamma_2 / r. \quad [7]
 \end{aligned}$$

where γ_2 is an arbitrary constant,

$$\begin{aligned}
 \frac{d}{dr} \{ [(3 \cos \alpha - \cos^3 \alpha) (n_1 T_1^{3/2} - n_2 T_2^{3/2})] + \frac{1}{\sqrt{2\pi R}} [(3\pi - 6\alpha + 4 \sin 2\alpha - \frac{\sin 4\alpha}{2}) n_1 V_1 T_1 \\
 + (3\pi + 6\alpha - 4 \sin 2\alpha + \frac{\sin 4\alpha}{2}) n_2 V_2 T_2] \} + \frac{1}{r} [(3 \cos \alpha - 2 \cos^3 \alpha) (n_1 T_1^{3/2} - n_2 T_2^{3/2})]
 \end{aligned}$$

Free cylindrical Couette flow of a rarefied GAS with heat..

$$\begin{aligned}
 & + \frac{2}{r} \frac{1}{\sqrt{2\Pi R}} [(\Pi - 2\alpha + 2 \sin 2\alpha - \frac{3}{4} \sin 4\alpha) n_1 v_1 T_1 + \\
 & + (\Pi + 2\alpha - 2 \sin 2\alpha + \frac{3}{4} \sin 4\alpha) n_2 v_2 T_2] = 0, \quad [8]
 \end{aligned}$$

$$\begin{aligned}
 & \cos^3 \alpha (n_1 T_1^{3/2} - n_2 T_2^{3/2}) + \frac{1}{\sqrt{2\Pi R}} [(\Pi - 2\alpha + \frac{\sin 4\alpha}{2}) n_1 v_1 T_1 + \\
 & + (\Pi + 2\alpha - \frac{\sin 4\alpha}{2}) n_2 v_2 T_2] = \gamma_3 / r^3, \quad [9]
 \end{aligned}$$

γ_3 is an arbitrary constant.

and

$$\begin{aligned}
 & \frac{d}{dr} \left\{ \left[(\Pi - 2\alpha + \frac{\sin 4\alpha}{2}) n_1 T_1^2 + (\Pi + 2\alpha - \frac{\sin 4\alpha}{2}) n_2 T_2^2 \right] + \right. \\
 & + 8 \sqrt{\frac{2\Pi}{R}} \left[(5 \cos^3 \alpha - 3 \cos^5 \alpha) (n_1 v_1 T_1^{3/2} - n_2 v_2 T_2^{3/2}) \right] \left. \right\} + \\
 & + \frac{2(\sin 4\alpha - 2 \sin 2\alpha)}{r} [n_1 T_1^2 - n_2 T_2^2] + \\
 & + \frac{24}{R} \sqrt{\frac{2\Pi}{R}} \left[(5 \cos^3 \alpha - 4 \cos^5 \alpha) (n_1 v_1 T_1^{3/2} - n_2 v_2 T_2^{3/2}) \right] = 0. \quad [10]
 \end{aligned}$$

The boundary conditions on f leads to the following conditions in the case when the reflection coefficient is arbitrary.

$$f_1(R_1) = (1 - \epsilon) [-f_2(R_2)] + \epsilon f_{s_1},$$

$$f_2(R_2) = (1 - \epsilon) [-f_1(R_1)] + \epsilon f_{s_2}.$$

where,

$$f_{s_1} = \frac{n_{s_1}}{(2\Pi RT_{s_1})^{3/2}} \left(1 + \frac{a}{RT_{s_1}} C_r \right) e^{-C^2/2RT_{s_1}},$$

$$f_{s_2} = \frac{n_{s_2}}{(2\Pi RT_{s_2})^{3/2}} \left(1 + \frac{a}{RT_{s_2}} C_r \right) e^{-C^2/2RT_{s_2}}$$

Free cylindrical Couette flow of a rarefied GAS with heat..

and

$$\begin{aligned} & \left\{ \frac{3R}{2\pi} (\Pi+2\alpha_1)n_2(R_2)T_2(R_2) - 4\sqrt{\frac{R}{2\pi}} \cos\alpha_1 n_2(R_2)V_2(R_2) \sqrt{T_2(R_2)} \right\} = \\ & = (1-\varepsilon) \left\{ \frac{3R}{2\pi} (\Pi+2\alpha_1)n_1(R_1)T_1(R_1) + 4\sqrt{\frac{R}{2\pi}} \cos\alpha_1 n_1(R_1)V_1(R_1)\sqrt{T_1(R_1)} \right\} + \\ & + \varepsilon \left\{ \frac{3R}{2\pi} (\Pi+2\alpha_1) n_{s_2} T_{s_2} - 4\sqrt{\frac{R}{2\pi}} \cos\alpha_1 n_{s_2} a \sqrt{T_{s_2}} \right\}, \quad [16] \end{aligned}$$

where, $n_{s_2} = n_s$, $T_{s_2} = T_s$, $T_{s_1} = T_s (1+x)$. and R_1, R_2 are the radii of inner and outer cylinders and T_s is the temperature of the outer cylinder. The inner cylinder was considered fixed and its temperature differs from the temperature of the outer cylinder by $X T_s$. The quantity X is taken small, so that we can neglect its square.

If, we take in nondimensional form the quantities

$$\begin{aligned} V_1 &= V_1' a, & V_2 &= V_2' a, & n_1 &= n_1' n_s, & n_s &= n_2' n_s \\ r &= r' R_2, & T_1 &= T_1' T_s, & T_2 &= T_2' T_s, & \cos\alpha &= \frac{R_1}{r' R_2} \\ q &= \frac{R_1}{R_2}, & \cos\alpha_0 &= 1, & \alpha_0 &= 0, & \cos\alpha_1 &= q \end{aligned}$$

The system of equations [5]-[16] in nondimensional form after dropping the primes will be

$$[n_1 T_1^{1/2} - n_2 T_2^{1/2}] + \eta [(\Pi - 2\alpha + \sin 2\alpha) n_1 V_1 + (\Pi + 2\alpha - \sin 2\alpha) n_2 V_2] r = \gamma_1, \quad [17]$$

$$\begin{aligned} \frac{d}{dr} \left\{ [(\Pi - 2\alpha + \sin 2\alpha) n_1 T_1 + (\Pi + 2\alpha - \sin 2\alpha) n_2 T_2] + \frac{\beta_1 (3r^2 - q^2)}{r^3} (n_1 V_1 T_1^{1/2} - n_2 V_2 T_2^{1/2}) \right\} \\ + \frac{4 \sin 2\alpha}{r} (n_1 T_1 - n_2 T_2) + \frac{\beta_1}{r} \frac{(3r^2 - q^2)}{r^3} (n_1 V_1 T_1^{1/2} - n_2 V_2 T_2^{1/2}) = 0, \quad [18] \end{aligned}$$

$$[n_1 T_1^{3/2} - n_2 T_2^{3/2}] + \frac{5\eta}{4} \{ (\Pi - 2\alpha + \sin 2\alpha) n_1 V_1 T_1 + (\Pi + 2\alpha - \sin 2\alpha) n_2 V_2 T_2 \} r = \gamma_2, \quad [19]$$

$$\frac{d}{dr} \left\{ \left[\frac{(3r^2 - q^2)}{r^3} (n_1 T_1^{3/2} - n_2 T_2^{3/2}) \right] + \eta \left[(3\Pi - 6\alpha + 4 \sin 2\alpha - \frac{\sin 4\alpha}{2}) n_1 V_1 T_1 + \right. \right.$$

By multiplying the last two equations by dC , $C_T dC$ and $C^2 dC$ respectively and integrating, we get:

$$\begin{aligned} & \left[\sqrt{2\pi R^3}(\pi - 2\alpha_0) + 4\pi R \cos \alpha_0 \frac{V_1(R_1)}{\sqrt{T_1(R_1)}} \right] n_1(R_1) = \\ & = (1-\epsilon) \left[-\sqrt{2\pi R^3}(\pi - 2\alpha_0) - 4\pi R \cos \alpha_0 \frac{V_2(R_2)}{\sqrt{T_2(R_2)}} \right] n_2(R_2) \\ & + \epsilon \left[\sqrt{2\pi R^3}(\pi - 2\alpha_0) + 4\pi R \cos \alpha_0 \frac{a}{\sqrt{T_{S_1}}} \right] n_{S_1}, \end{aligned} \quad [11]$$

$$\begin{aligned} & \left[\sqrt{2\pi R^3}(\pi + 2\alpha_1) - 4\pi R \cos \alpha_1 \frac{V_2(R_2)}{\sqrt{T_2(R_2)}} \right] n_2(R_2) = \\ & = (1-\epsilon) \left[-\sqrt{2\pi R^3}(\pi + 2\alpha_1) + 4\pi R \cos \alpha_1 \frac{V_1(R_1)}{\sqrt{T_1(R_1)}} \right] n_1(R_1) + \\ & + \epsilon \left[\sqrt{2\pi R^3}(\pi + 2\alpha_1) - 4\pi R \cos \alpha_1 \frac{a}{\sqrt{T_{S_2}}} \right] n_{S_2}, \end{aligned} \quad [12]$$

$$\begin{aligned} & \{ 2\pi R^2 \cos \alpha_0 n_1(R_1) \sqrt{T_1(R_1)} + \sqrt{2\pi R^3}(\pi - 2\alpha_0 + \sin 2\alpha_0) n_1(R_1) V_1(R_1) \} = \\ & = (1-\epsilon) \{ -2\pi R^2 \cos \alpha_0 n_2(R_2) \sqrt{T_2(R_2)} - \sqrt{2\pi R^3}(\pi - 2\alpha_0 + \sin 2\alpha_0) n_2(R_2) V_2(R_2) \} \\ & + \epsilon \{ 2\pi R^2 \cos \alpha_0 n_{S_1} \sqrt{T_{S_1}} + \sqrt{2\pi R^3}(\pi - 2\alpha_0 + \sin 2\alpha_0) a n_{S_1} \}, \end{aligned} \quad [13]$$

$$\begin{aligned} & \{ 2\pi R^2 \cos \alpha_1 n_2(R_2) \sqrt{T_2(R_2)} - \sqrt{2\pi R^3}(\pi + 2\alpha_1 - \sin 2\alpha_1) n_2(R_2) V_2(R_2) \} = \\ & = (1-\epsilon) \{ -2\pi R^2 \cos \alpha_1 n_1(R_1) \sqrt{T_1(R_1)} + \sqrt{2\pi R^3}(\pi + 2\alpha_1 - \sin 2\alpha_1) n_1(R_1) V_1(R_1) \} \\ & + \epsilon \{ 2\pi R^2 \cos \alpha_1 n_{S_2} \sqrt{T_{S_2}} - \sqrt{2\pi R^3}(\pi + 2\alpha_1 - \sin 2\alpha_1) a n_{S_2} \}, \end{aligned} \quad [14]$$

$$\begin{aligned} & \left\{ \frac{3R}{2\pi}(\pi - 2\alpha_0) n_1(R_1) T_1(R_1) + 4 \sqrt{\frac{R}{2\pi}} \cos \alpha_0 n_1(R_1) V_1(R_1) \sqrt{T_1(R_1)} \right\} = \\ & = (1-\epsilon) \left\{ \frac{-3R}{2\pi}(\pi - 2\alpha_0) n_2(R_2) T_2(R_2) - 4 \sqrt{\frac{R}{2\pi}} \cos \alpha_0 n_2(R_2) V_2(R_2) \sqrt{T_2(R_2)} \right\} \\ & + \epsilon \left\{ \frac{3R}{2\pi}(\pi - 2\alpha_0) n_{S_1} T_{S_1} + 4 \sqrt{\frac{R}{2\pi}} \cos \alpha_0 n_{S_1} a \sqrt{T_{S_1}} \right\}, \end{aligned} \quad [15]$$

$$+(3\Pi+6\alpha-4\sin 2\alpha+\frac{\sin 4\alpha}{2})n_2V_2T_2\} + \frac{(3r^2-q^2)}{r^4}(n_1T_1^{3/2}-n_2T_2^{3/2}) +$$

$$+\frac{2\eta}{r}[(\Pi-2\alpha+2\sin 2\alpha-\frac{3}{4}\sin 4\alpha)n_1V_1T_1+(\Pi+2\alpha-2\sin 2\alpha+\frac{3}{4}\sin 4\alpha)n_2V_2T_2]=0, \quad [20]$$

$$\frac{q^3}{r^3}[n_1T_1^{3/2}-n_2T_2^{3/2}]+\eta[(\Pi+2\alpha+\frac{\sin 4\alpha}{2})n_1V_1T_1+(\Pi+2\alpha-\frac{\sin 4\alpha}{2})n_2V_2T_2]=\frac{\gamma_3}{r^3}, \quad [21]$$

$$\frac{d}{dr}\{[(\Pi-2\alpha+\frac{1}{2}\sin 4\alpha)n_1T_1^2+(\Pi+2\alpha-\frac{1}{2}\sin 4\alpha)n_2T_2^2]\} +$$

$$+\frac{8\beta_1q^2}{r^5}(5r^2-3q^2)(n_1V_1T_1^{3/2}-n_2V_2T_2^{3/2}) + \frac{2(\sin 4\alpha-2\sin 2\alpha)}{r}[n_1T_1^2-n_2T_2^2] +$$

$$+\frac{24\beta_1q^2}{r^6}[(5r^2-4q^2)(n_1V_1T_1^{3/2}-n_2V_2T_2^{3/2})] = 0, \quad [22]$$

where, $\eta = \frac{a}{q\sqrt{2\Pi RT_s}}$, $\beta_1 = \sqrt{\frac{2}{RT_s}} a q$.

Under the boundary conditions

$$[1+4\eta q \frac{V_1(q)}{\sqrt{T_1(q)}}]n_1(q) = (1-\epsilon)[-1-4\eta q \frac{V_2(1)}{\sqrt{T_2(1)}}]n_2(1) + \epsilon[1 + \frac{4\eta q}{\sqrt{1+X}}], \quad [23]$$

$$[(\Pi+2\alpha)-2\beta_1 \frac{V_2(1)}{\sqrt{T_2(1)}}]n_2(1) = (1-\epsilon)[-(\Pi+2\alpha_1)+2\beta_1 \frac{V_1(q)}{\sqrt{T_1(q)}}]n_1(q) +$$

$$+[(\Pi+2\alpha_1)-2\beta_1], \quad [24]$$

$$[n_1(q)\sqrt{T_1(q)}+\Pi\eta n_1(q)V_1(q)] = (1-\epsilon)[-n_2(1)\sqrt{T_2(1)}-\Pi\eta n_2(1)V_2(1)] +$$

$$+\epsilon[\sqrt{1+X} + \Pi\eta], \quad [25]$$

$$[n_2(1)\sqrt{T_2(1)}-\eta(\Pi+2\alpha_1-\sin 2\alpha_1)n_2(1)V_2(1)] = (1-\epsilon)[-n_1(q)\sqrt{T_1(q)} +$$

$$+\eta(\Pi+2\alpha_1-\sin 2\alpha_1)n_1(q)V_1(q)] + \epsilon[1-\eta(\Pi+2\alpha_1-\sin 2\alpha_1)], \quad [26]$$

$$[\frac{3}{2}n_1(q)T_1(q)+4\eta q n_1(q)V_1(q)\sqrt{T_1(q)}]=$$

Free cylindrical Couette flow of a rarefied GAS with heat..

$$\begin{aligned}
 &= (1-\epsilon) \left[-\frac{3}{2} n_2(1) T_2(1) - 4\eta q n_2(1) v_2(1) \sqrt{T_2(1)} \right] + \\
 &+ \epsilon \left[\frac{3}{2} (1+X) + 4\eta q \sqrt{1+X} \right], \quad [27]
 \end{aligned}$$

$$\begin{aligned}
 &\left[\frac{3}{2} (\Pi + 2\alpha_1) n_2(1) T_2(1) - 4q^2 \eta n_2(1) v_2(1) \sqrt{T_2(1)} \right] = \\
 &= (1-\epsilon) \left\{ -\frac{3}{2} (\Pi + 2\alpha_1) n_1(q) T_1(q) + 4q^2 \eta n_1(q) v_1(q) \sqrt{T_1(q)} + \right. \\
 &\left. + \epsilon \left\{ \frac{3}{2} (\Pi + 2\alpha_1) - 4q^2 \eta \right\} \right\}. \quad [28]
 \end{aligned}$$

Equations [17]-[22] are nonlinear, X is small.

Now, we discuss the following two cases:

Case 1: If $v_1 = v_2 = 0$

In this case, we put.

$$n_1 = 1 + X n_1^{(1)}, \quad n_2 = 1 + X n_2^{(1)}$$

$$T_1 = 1 + X T_1^{(1)}, \quad T_2 = 1 + X T_2^{(1)},$$

$$\text{and } \gamma_1 = 1 + X \gamma_1^{(1)}$$

On substituting these values in equations [17],[18],[20] and [22] equating the coefficients of X on both sides in the resulting equations, we get:

$$n_1^{(1)} + \frac{1}{2} T_1^{(1)} - n_2^{(1)} - \frac{1}{2} T_2^{(1)} = \gamma_1^{(1)} \quad [17]'$$

$$\begin{aligned}
 &\frac{d}{dr} \left\{ [(\Pi - 2\alpha + \sin 2\alpha)(n_1^{(1)} + T_1^{(1)}) + (\Pi + 2\alpha - \sin 2\alpha)(n_2^{(1)} + T_2^{(1)})] \right\} \\
 &+ \frac{4\sin 2\alpha}{r} [n_1^{(1)} + T_1^{(1)} - n_2^{(1)} - T_2^{(1)}] = 0, \quad [18]'
 \end{aligned}$$

$$\frac{d}{dr} \left\{ \frac{(3r^2 - q^2)}{r^3} (n_1^{(1)} + \frac{3}{2} T_1^{(1)} - n_2^{(1)} - \frac{3}{2} T_2^{(1)}) \right\} +$$

Khidr, Abourabia & Mahmoud.

$$+ \frac{1}{r} \left(\frac{3r^2 - q^2}{r^3} \right) (n_1^{(1)} + \frac{3}{2} T_1^{(1)} - n_2^{(1)} - \frac{3}{2} T_2^{(1)}) = 0, \quad [20]$$

and

$$\frac{d}{dr} \{ (\Pi - 2\alpha + \frac{1}{2} \sin 4\alpha) (n_1^{(1)} + 2T_1^{(1)}) + (\Pi + 2\alpha - \frac{1}{2} \sin 4\alpha) (n_2^{(1)} + 2T_2^{(1)}) \} + \frac{2(\sin 4\alpha - 2\sin 2\alpha)}{r} [n_1^{(1)} + 2T_1^{(1)} - n_2^{(1)} - 2T_2^{(1)}] = 0. \quad [22]$$

The above equations are valid under the following boundary conditions:

$$\begin{aligned} n_1^{(1)}(q) = 0 & , & n_2^{(1)}(1) = 0 \\ T_1^{(1)}(q) = \frac{1}{(2-\epsilon)} & , & T_2^{(1)}(1) = \frac{(\epsilon-1)}{(2-\epsilon)} \end{aligned} \quad [29]$$

For α is sufficiently small ($\alpha \ll 1$), the solution of the system of equations [17], [18], [20] and [22] gives

$$n_1^{(1)} = \frac{1}{2} \left\{ \left(\frac{3}{2} \gamma_1^{(1)} + 2A_1 - A_3 \right) - \frac{r^2}{2(3r^2 - q^2)} A_2 \right\}, \quad [30]$$

$$n_2^{(1)} = \frac{1}{2} \left\{ (2A_1 - A_3 - \frac{3}{2} \gamma_1^{(1)}) + \frac{r^2}{2(3r^2 - q^2)} A_2 \right\}, \quad [31]$$

$$T_1^{(1)} = \frac{1}{2} \left\{ (A_3 - A_1 - \gamma_1^{(1)}) + \frac{r^2}{(3r^2 - q^2)} A_2 \right\}, \quad [32]$$

and

$$T_2^{(1)} = \frac{1}{2} \left\{ (\gamma_1^{(1)} - A_1 + A_3) - \frac{r^2}{(3r^2 - q^2)} A_2 \right\}, \quad [33]$$

where, A_1 , A_2 and A_3 are the integration constants and can be determined by using the boundary conditions [29], where

$$\gamma_1^{(1)} = \frac{1}{2}, \quad A_1 = \frac{(5-q^2)(6+\epsilon) - 6(2-\epsilon)(3-q^2)}{4(2-\epsilon)(5-q^2)},$$

$$A_2 = \frac{6(3q^2)}{(5-q^2)}, \quad A_3 = \frac{(18-\epsilon)(5-q^2) - 18(2-\epsilon)(3-q^2)}{4(2-\epsilon)(5-q^2)}$$

Free cylindrical Couette flow of a rarefied GAS with heat..

Case 2: In this case we assume that V is of order of the Mach number, i.e.,

$$\begin{aligned} V_i &= M V_{iR} & , & \quad T_i = 1 + X T_i^{(1)} + M T_i^{(2)}, \\ n_i &= 1 + X n_i^{(1)} + M n_i^{(2)} & , & \quad \gamma_1 = 1 + X \gamma_1^{(1)} + M \gamma_1^{(2)}, \\ \gamma_2 &= M \gamma_2^{(2)}, \quad \gamma_3 = M \gamma_3^{(2)}, & \text{i.e. } & M^2 \ll 1 \text{ and } XM \ll 1. \end{aligned} \quad [34]$$

For α is sufficiently small, then $\sin \alpha = \alpha$, $q = 1$.

On substituting these values in equations [17]-[22] and on boundary conditions [23]-[28] and equating the coefficient of M on both sides of the resulting equations we get:

$$(n_1^{(2)} + \frac{1}{2} T_1^{(2)} - n_2^{(2)} - \frac{1}{2} T_2^{(2)}) + \Pi \eta (V_{1R} + V_{2R}) = \gamma_1^{(2)}. \quad [35]$$

$$\frac{d}{dr} \{ n_1^{(2)} + T_1^{(2)} + n_2^{(2)} + T_2^{(2)} \} + \frac{\beta_1}{\Pi} \frac{(3r^2-1)}{r^4} (V_{1R} - V_{2R}) = 0, \quad [36]$$

$$(n_1^{(2)} + \frac{3}{2} T_1^{(2)} - n_2^{(2)} - \frac{3}{2} T_2^{(2)}) + \frac{5\Pi\eta}{4} r (V_{1R} + V_{2R}) = \gamma_2^{(2)} \quad [37]$$

$$\begin{aligned} \frac{d}{dr} \left\{ \frac{(3r^2-1)}{r^3} (n_1^{(2)} + \frac{3}{2} T_1^{(2)} - n_2^{(2)} - \frac{3}{2} T_2^{(2)}) + 3\eta (V_{1R} + V_{2R}) \right\} + \\ + \left[\frac{(3r^2-1)}{r^4} (n_1^{(2)} + \frac{3}{2} T_1^{(2)} - n_2^{(2)} - \frac{3}{2} T_2^{(2)}) + \frac{2\Pi\eta}{r} (V_{1R} + V_{2R}) \right] = 0, \end{aligned} \quad [38]$$

$$\frac{1}{r^3} (n_1^{(2)} + \frac{3}{2} T_1^{(2)} - n_2^{(2)} - \frac{3}{2} T_2^{(2)}) + \eta \Pi (V_{1R} + V_{2R}) = \frac{\gamma_3^{(2)}}{r^3}, \quad [39]$$

$$\begin{aligned} \frac{d}{dr} \left\{ (n_1^{(2)} + 2T_1^{(2)} + n_2^{(2)} + 2T_2^{(2)}) + \frac{8\beta_1}{\Pi r^3} (5r^2-3)(V_{1R} - V_{2R}) \right\} + \\ + \frac{24\beta_1}{\Pi r^6} [(5r^2-4)(V_{1R} - V_{2R})] = 0 \end{aligned} \quad [40]$$

Free cylindrical couette flow of a rarefied GAS with heat..

in the boundary conditions [41]-[46] and equating the terms free of q on both sides and equating the terms containing q on both sides, one obtains a system of boundary conditions.

If, we consider $n_2^{(2)}$, $T_2^{(2)}$ depend only on ρ and ρ^2 , then, $C_3=C_3'=0$.

The solution of the resulting system of equations gives:

$$C_1 = 7\gamma_3^{(2)} - \frac{15}{2}\alpha_2^{(2)} + \frac{3}{2}\alpha_1^{(2)}, \quad C_2 = (242\alpha_2^{(2)} - \frac{233}{2}\alpha_3^{(3)}),$$

$$C_3 = 0, \quad C_4 = (238\gamma_2^{(2)} - \frac{159}{2}\gamma_3^{(2)}),$$

$$C_5 = -(3177\gamma_2^{(2)} + 3669\gamma_3^{(2)}), \quad C_6 = -(3679\gamma_2^{(2)} + 3737\gamma_3^{(2)}),$$

$$C_1' = (\gamma_3^{(2)} - \gamma_1^{(2)}), \quad C_2' = (64\gamma_3^{(2)} - \frac{455}{2}\gamma_2^{(2)}),$$

$$C_3' = 0, \quad C_4' = (104\gamma_3^{(2)} - \frac{465}{2}\gamma_2^{(2)}),$$

$$C_5' = (3523\gamma_2^{(2)} + 3837\gamma_3^{(2)}), \quad C_6' = (3387\gamma_2^{(2)} + 3763\gamma_3^{(2)}),$$

$$C_1'' = \frac{(\frac{99}{10}\gamma_2^{(2)} - 11\gamma_3^{(2)})}{\Pi\eta}, \quad C_2'' = \frac{(31\gamma_2^{(2)} - 36\gamma_3^{(2)})}{\Pi\eta},$$

$$C_3'' = \frac{370\gamma_2^{(2)} - 6\gamma_3^{(2)}}{\Pi\eta}, \quad C_4'' = \frac{(41\gamma_3^{(2)} - 36\gamma_2^{(2)})}{\Pi\eta},$$

$$C_5'' = \frac{-370\gamma_2^{(2)} - 723\gamma_3^{(2)}}{\Pi\eta}, \quad C_6'' = \frac{627\gamma_3^{(2)} - 20\gamma_2^{(2)}}{\Pi\eta}$$

where $\gamma_1^{(2)}$, $\gamma_2^{(2)}$ and $\gamma_3^{(2)}$ can be written in the form

$$\gamma_1^{(2)} = \frac{8(\Pi\eta - 8\eta - 1) + \Pi\epsilon(3 - 8\eta)}{2(2 - \epsilon)(3\Pi - 8)},$$

$$\gamma_2^{(2)} = \frac{192\eta(\Pi - 4) + 5\Pi\epsilon(3 - 8\eta)}{8(2 - \epsilon)(3\Pi - 8)},$$

$$\gamma_3^{(2)} = \frac{16\eta(3\Pi - 2) + \Pi\epsilon(3 - 8\eta)}{2(2 - \epsilon)(3\Pi - 8)},$$

The above equations are valid under the following boundary conditions:

$$[n_1^{(2)} + 3\eta V_{1r}(q)] = (1-\epsilon)[-n_2^{(2)}(1) - 4\eta V_{2r}(1)] - \epsilon(2\eta), \quad [41]$$

$$[\Pi n_2^{(2)}(1) - 2\beta_1 V_{2r}(1)] = (1-\epsilon)[- \Pi n_1^{(2)}(q) + 2\beta_1 V_{1r}(q)], \quad [42]$$

$$[(n_1^{(2)} + \frac{1}{2}T_1^{(2)}) + \Pi\eta V_{1r}(q)] = (1-\epsilon)[-(n_2^{(2)} + \frac{1}{2}T_2^{(2)}) - \Pi\eta V_{2r}(1) + \epsilon/2], \quad [43]$$

$$[(n_2^{(2)} + \frac{1}{2}T_2^{(2)}) - \Pi\eta V_{2r}(1)] = (1-\epsilon)[-(n_1^{(2)} + \frac{1}{2}T_1^{(2)}) + \Pi\eta V_{1r}(q)], \quad [44]$$

$$[\frac{3}{2}(n_1^{(2)} + T_1^{(2)}) + 4\eta V_{1r}(q)] = (1-\epsilon)[-\frac{3}{2}(n_2^{(2)} + T_2^{(2)}) - 4\eta V_{2r}(1)] + \epsilon(2\eta), \quad [45]$$

and

$$[\frac{3}{2}\Pi(n_2^{(2)} + T_2^{(2)}) - 4\eta V_{2r}(1)] = (1-\epsilon)[-\frac{3}{2}\Pi(n_1^{(2)} + T_1^{(2)}) + 4\eta V_{1r}(q)]. \quad [46]$$

On substituting $r = 1 - \rho$, $\rho^3 \ll 1$

$$n_1^{(2)} = C_1 + C_2\rho + C_5\rho^2, \quad n_2^{(2)} = C_3 + C_4\rho + C_6\rho^2,$$

$$T_1^{(2)} = C'_1 + C'_2\rho + C'_5\rho^2, \quad T_2^{(2)} = C'_2 + C'_4\rho + C'_6\rho^2,$$

$$V_{1r} = C''_1 + C''_2\rho + C''_5\rho^2, \quad V_{2r} = C''_3 + C''_3\rho + C''_6\rho^2.$$

in equations [35]-[40] by equating the terms free of ρ on both sides, equating the terms containing ρ on both sides and equating the terms containing ρ^2 on both sides and by solving the resulting system of equations, and on substituting

$$\rho = 0, \quad \rho = 1-q$$

$$n_1^{(2)} = C_1 + C_2(1-q), \quad T_1^{(2)} = C'_1 + C'_2(1-q), \quad V_{1r} = C''_1 + C''_2(1-q)$$

$$n_2^{(2)} = C_3, \quad T_2 = C'_3, \quad V_{2r} = C''_3,$$

then

$$n_1^{(2)} = (7\gamma_3^{(2)} - \frac{15}{2}\gamma_2^{(2)} + \frac{3}{2}\gamma_1^{(2)}) + (242\gamma_2^{(2)} - \frac{233}{2}\gamma_3^{(2)})\rho - (3177\gamma_2^{(2)} + 3669\gamma_3^{(2)})\rho^2,$$

$$n_2^{(2)} = (238\gamma_2^{(2)} - \frac{159}{2}\gamma_3^{(2)})\rho - (3679\gamma_2^{(2)} + 3727\gamma_3^{(2)})\rho^2,$$

$$T_1^{(2)} = (\gamma_3^{(2)} - \gamma_1^{(2)}) + (64\gamma_3^{(2)} - \frac{455}{2}\gamma_2^{(2)})\rho + (3525\gamma_2^{(2)} + 3837\gamma_3^{(2)})\rho^2.$$

$$T_2^{(2)} = (104\gamma_3^{(2)} - \frac{465}{2}\gamma_2^{(2)})\rho + (3387\gamma_2^{(2)} + 3763\gamma_3^{(2)})\rho^2,$$

$$V_{1r} = \frac{1}{\Pi\eta} \{ (\frac{99}{10}\gamma_2^{(2)} - 11\gamma_3^{(2)}) + (31\gamma_2^{(2)} - \frac{3}{10}\gamma_3^{(2)})\rho - (370\gamma_2^{(2)} + 723\gamma_3^{(2)})\rho^2 \},$$

and

$$V_{2r} = \frac{1}{\Pi\eta} \{ (7\gamma_3^{(2)} - 6\gamma_2^{(2)}) + (41\gamma_3^{(2)} - 36\gamma_2^{(2)})\rho - (627\gamma_3^{(2)} - 201\gamma_2^{(2)})\rho^2 \}.$$

For $r=1-\rho$, $q=1$, $\rho^3 \ll 1$, the zeroth approximation of the density and the temperature are

$$n=1 + \frac{3X\alpha}{4\Pi} \rho,$$

$$T = \frac{1}{n} [1 + \frac{X}{2} (\frac{\epsilon}{2-\epsilon})],$$

and the first approximation of the density, mean velocity and the temperature are

$$n=1 + \frac{3X\alpha}{4\Pi} \rho + M[\frac{3}{4}\gamma_1^{(2)} + \frac{25}{4}\gamma_2^{(2)} - 8\gamma_3^{(2)}] + \frac{(2923\gamma_2^{(2)} - 1333\gamma_3^{(2)})}{10} \rho]$$

$$- \alpha_1 \frac{M}{\Pi} [(7\gamma_3^{(2)} - \frac{15}{2}\gamma_2^{(2)} + \frac{3}{2}\gamma_1^{(2)}) + (4\gamma_2^{(2)} - 32\gamma_3^{(2)})\rho]. \quad [47]$$

$$V_r = \frac{\eta}{2\Pi n} \{ (x/16)[8-\rho] + M[(\frac{15}{2}\gamma_3^{(2)} - \frac{15}{2}\gamma_2^{(2)} + \gamma_1^{(2)}) + (\gamma_1^{(2)} - \gamma_2^{(2)} - \frac{89}{2}\gamma_3^{(2)})\rho] \} +$$

$$+ \frac{M}{2\Pi\eta n} [(\frac{39}{10}\gamma_2^{(2)} - 4\gamma_3^{(2)}) + (\frac{407}{10}\gamma_3^{(2)} - 5\gamma_2^{(2)})\rho] \quad [48]$$

$$T = \frac{1}{n} [1 + \frac{X}{2} [\frac{\epsilon}{2-\epsilon}] + M[(\frac{1}{4}\gamma_1^{(2)} + \frac{25}{2}\gamma_2^{(2)} - \frac{15}{2}\gamma_3^{(2)}) +$$

$$+ (\frac{527}{10}\gamma_2^{(2)} - \frac{378}{10}\gamma_3^{(2)})\rho]], \quad [49]$$

where η is the coefficient related to the velocity through the porous surface.

Free cylindrical Couette flow of a rarefied GAS with heat..

CONCLUSION:

The numerical investigation to the above results are illustrated in figures (1)-(4). The analysis of these results leads to:

(i) From Fig. (1), we see that the density decreases with the increase of ρ (distance between the two cylinders) for constant η (coefficient related to velocity through the porous surface) and reflection coefficient ϵ .

(ii) From Fig. (2), we see that the density decreases as ρ increases for constant η and ϵ , and it increases as η increases for constant ρ .

(iii) The magnitude of velocity increases with the increase of ρ for constant ϵ and it increases with the increase of ϵ for constant η as it is seen from Fig. (3).

(iv) From Fig. (4) the temperature at any point between the two cylinders increases as η increases for constant ϵ and ρ , and it increases as ϵ increases for constant η .

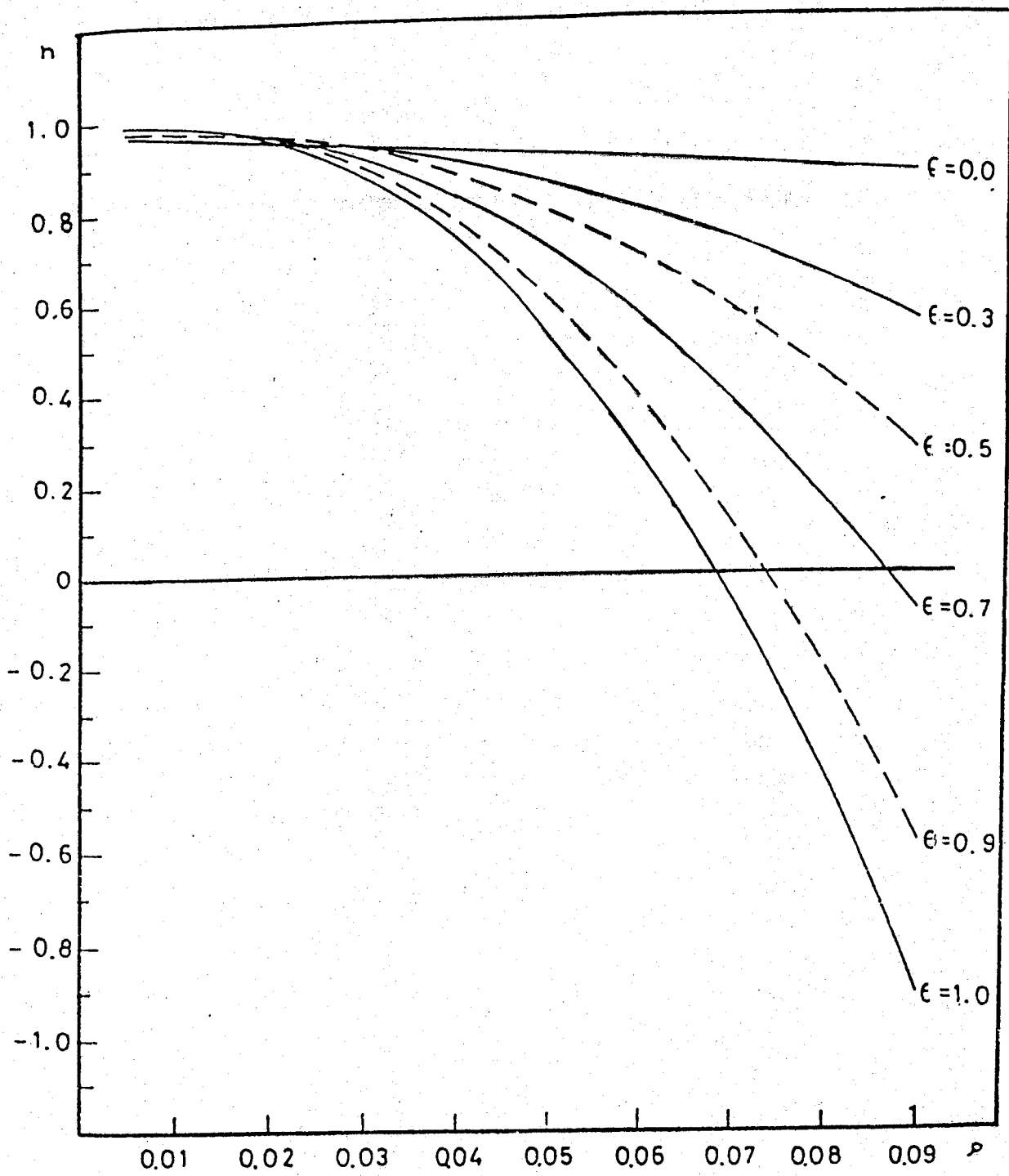


Fig. (1) Variation between density and distance ρ for constant ($\eta = 0.01$).

Free cylindrical Couette flow of a rarefied GAS with heat..

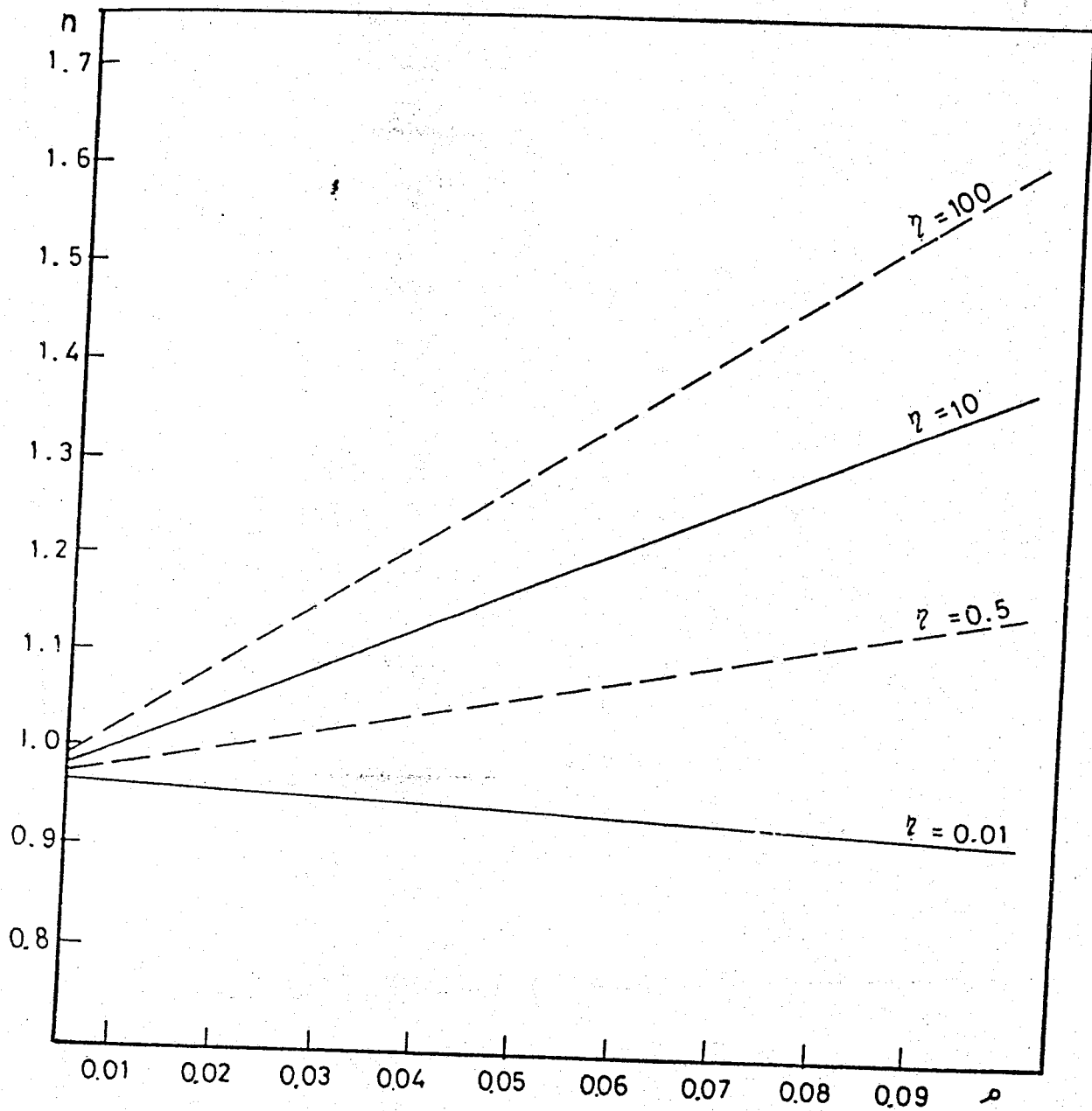


Fig. (2) Variation between density and distance ρ for constant ($\epsilon = 0.8$).

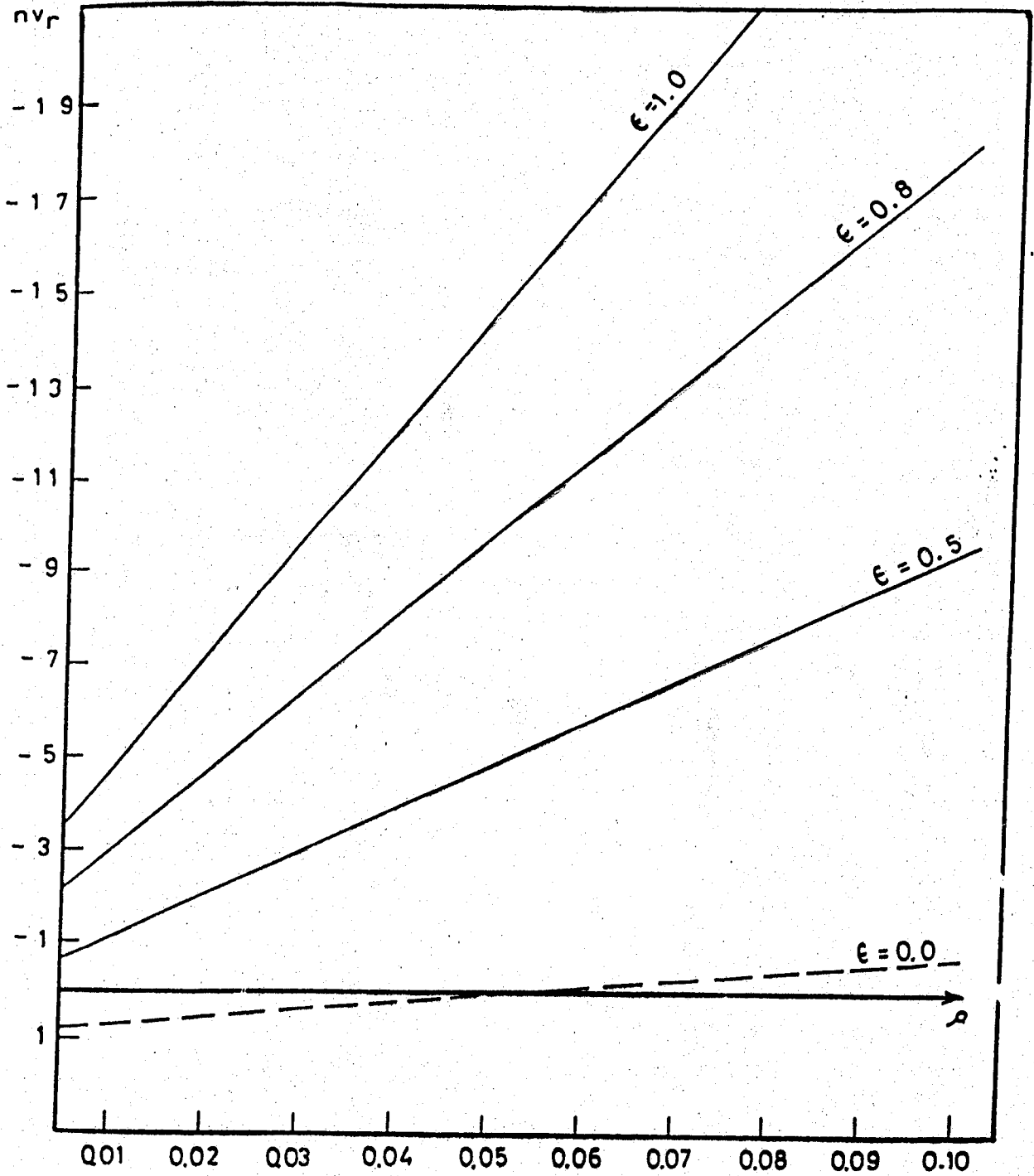


Fig. (3) Variation between nV_r and distance ρ for constant ($\eta = 0.01$).

Free cylindrical Couette flow of a rarefied GAS with heat..

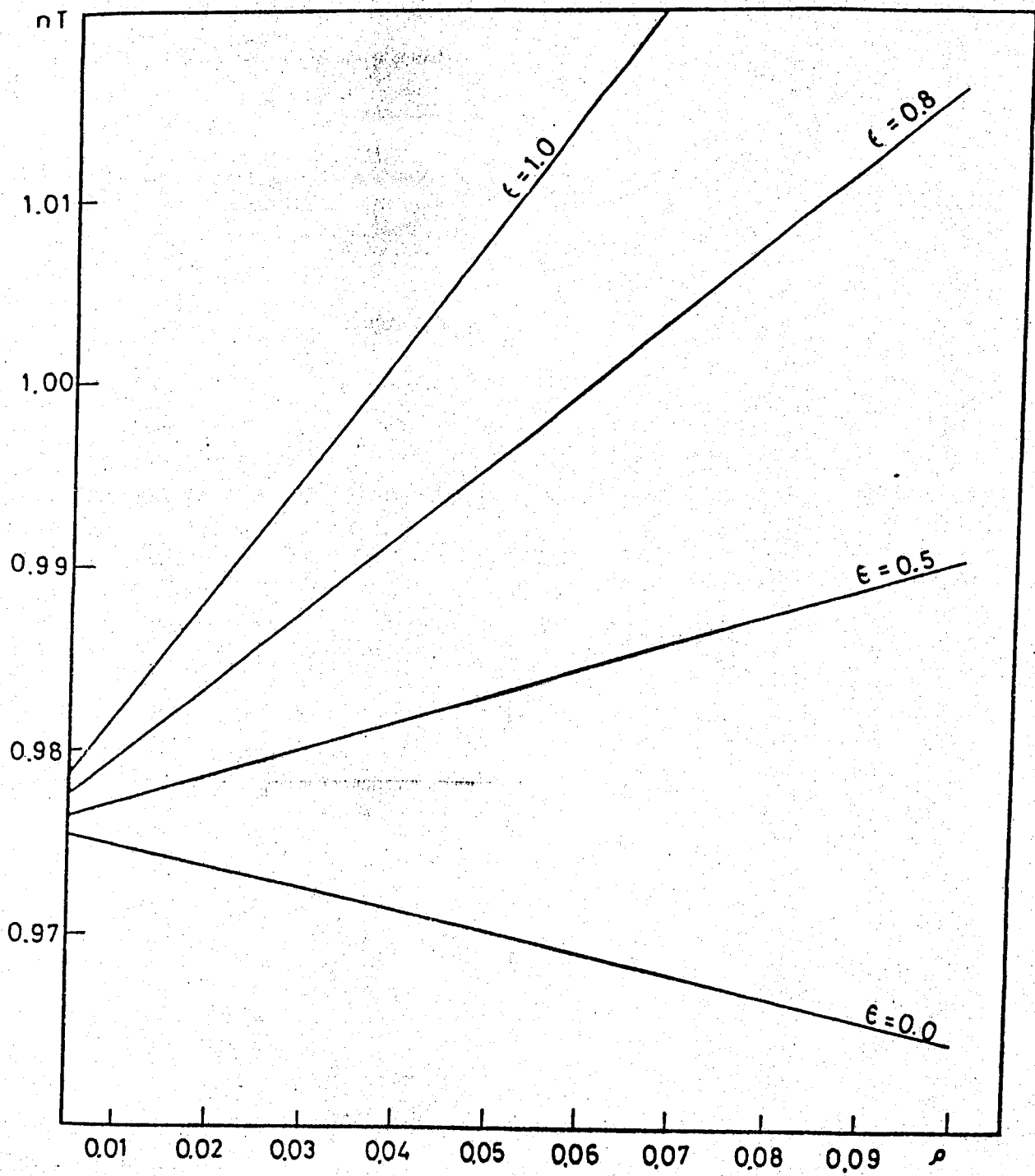


Fig. (4) Variation between nT and distance ρ for constant ($\eta = 0.01$).

Khidr, Abourabia & Mahmoud.

REFERENCES:

Abdel-Gaid M.A., Khidr M.A.: The kinetic theory description of flow over a cylinder at low speeds under constant force. *Revue Roumaine des sciences technique de mecanique appliquee*. V.24, No.5, pp. 699-706 (1979).

Galkin V.S.: The cylindrical Couette flow in a rarefied gas. *Inzhenerniy Zhurnal*, V.5, No.3 (1965). (in Russian).

Hady F.M.: Cylindrical Couette flow with heat transfer of a rarefied gas and porous surfaces. M.Sc. Assuit University. Egypt. (1976).

Khidr M.A., Abader A.A.: Heat transfer of an electron gas between two coaxial circular cylinders with arbitrary degree of rarefaction. *J. Math. and Phys. Soc. of Egypt*, No.41, pp.23-31(1979).