



Understanding of Visco-Elastic Surfactant And Acid Stimulation Application

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Abstract

Surfactants are divided into four main categories based on their ionic charge. The most common applications can be summarized as corrosion inhibitor, emulsifying and de-emulsifying agents, foaming agent and improver of solids carrying capacity. Visco-Elastic Surfactant (VES) is one of surfactant groups initially used as a friction reducer and to enhance the solids carrying capacity. In this paper many tests were performed on VES samples of newly produced product to study the work frame and the applicability of that product especially through three important factors 1) Viscosity build-up of the VES at different shear rates, 2) Study different concentrations behavior of the VES and its application especially on acid diversion, 3) Salt effect on the formed mixture of VES and its effect on the viscosity behavior, and finally 4) Temperature effect on the Visco-Elastic behavior was examined to define the work frame of that product (VES) application in the oil field in the acid diversion. VES product shows elasticity to stresses through the change in viscosity of the solution. Also, it was found that temperature affects negatively on the VES behavior, which limits the application of the VES in the high temperature reservoir, unless formation cooling action to be carried out before pumping the VES. On the other hand the salts have a positive effect on the VES behavior through increasing the viscosity buildup of the VES, which supports the application of VES in high saline formation water. The tested VES product shows good behavior as Visco-Elastic and could be used in limited temperature ranges, based on that result a case study was demonstrated in which it has been used as an acid diverter in carbonate reservoir. The well after the acid stimulation resulted in improving the well productivity and producing at 4100 BOPD after stimulation.

Keywords:

Surfactant; Visco-Elastic.

1. Introduction

1.1 Surfactants

There are four categories of surfactants a) anionic surfactant, b) cationic surfactant, c) nonionic surfactant & d) amphoteric surfactant. These four categories are classified based on its ionic group¹. Surfactant is composed of two main parts, head; which is the carrier of the ionic charge and the active part of the

surfactant and tail; that represent the hydrocarbon part of the surfactant and differs from surfactant to other on the no. of alkyls on group². Surfactants application usually depends on the ionic charge to support the purpose of application, for example in corrosion inhibitor, the cationic surfactant is used in cession inhibitor in order to be adsorbed on the tubular faces and cover it to form a film that helps preventing the acid attach to the tubular faces³.

Anionic surfactants are usually used as non-emulsifying agent or as friction reducer. Nonionic surfactant is the widely used surfactant as it doesn't react with the other chemicals or with the formation's mineral, it is used in improve the flow back and reducing the surface tension, and finally the amphoteric surfactant, in which VES is the main member of this group, Amphoteric surfactant is a surfactant that has positive and negative charge at the same time and tends to be positive under certain pH range⁴.

1.2 Acid Diversion

The success of matrix acidizing treatments depends on the placement of acid to remove near-wellbore formation damage efficiently. The acid should be placed so that all potentially productive intervals accept a sufficient quantity of the total acid volume. If significant permeability or formation damage variations are present in the interval to be treated, acid will enter the zones with the highest permeability or least formation damage, leaving little acid to treat what may be the most productive zones⁵. To achieve uniform damage removal, the original flow distribution across the treated interval needs to be altered to provide generally equal acid distribution. The methods used to alter this flow distribution are called diversion methods, since their purpose is to divert the flow of fluid from one portion of the interval being acidized to another⁶. The diversion method best suited for a particular situation depends on many factors, including the type of well completion, perforation density, the type of fluid that is produced or injected after the treatment, casing and cement sheath integrity, bottom hole temperature, and bottom hole pressure⁷. The best way to uniformly treat an interval is with a mechanical isolation device such as a straddle packer. This packer allows acid to be injected into small intervals, one by one, until the entire zone has been treated, however, this method is

often not practical or possible without a packer; diverting agents must be used during stimulation to reduce flow into nonproductive or undamaged zones and redirect this flow to zones in greater need of damage removal⁸.

1.3 Acid Diverters: Types and Uses

Acid diversion alters the natural flow profile into a formation during injection, causing acid flow to be diverted from undamaged or high permeability intervals to damaged or lower-permeability intervals⁹.

The diversion methods used to alter the original flow profile may attempt to achieve complete shutoff of flow into specific intervals or to equalize flow across the entire interval being treated, regardless of permeability or damage severity¹⁰. The types of diverting methods fall into four general categories:

- Ball sealers
- Degradable particulate-diverting agents
- Viscous fluids
- Foam

2. Experimental Work

A set of experiments were done to emphasize on the VES physical properties to stand on the frame of application, temperature range, viscosity build up, concentrations & range of acid strength.

2.1 Tools and Materials

The following apparatuses and equipments have been employed:-

- 1- BrookField viscometer to measure the viscosity of the fluid at different shear rates.
- 2- Acid resistance magnetic Stirrer.
- 3- Water bath.
- 4- pH meter.
- 5- pH caliber (Sulphonate solution with pH 7).
- 6- Glass ware.

The following materials have been used:-

- 1- 37.1 % Hydrochloric Acid ACS (American Chemistry Society).
- 2- CaCO₃ 93%.(ACS).
- 3- VES product with golden color, 0.99 Sp.Gr. & amphoteric ionic charge.

2.2 Study of Different VES Ratios in Acid Diversion

Optimization is always the main target in any work, as optimization seeks the cost control and high performance. Each surfactant has the optimum concentration at which the maximum benefit can be achieved. Determine the optimum ratio of the VES is really important to minimize the cost of the treatment and to avoid any unexpected formation damage could be a result of that extra dosage. The test was run with 13% HCl through applying different VES volume ratios 6, 7, 8 & 10% by volume, the test results shows in fig (1) that with higher VES concentration, higher viscosity build up of the VES gel at the same shear rate is achieved. That result was a guide for more application of the VES based on the target or fluid loss control. As it is known in fluid loss control higher viscosity is required to have a complete blockage of the targeted interval.

Also it shows the optimum application based on the formation permeability, as with higher permeable interval, higher viscosity is more desirable than lower viscosity. VES with 400 cp to 600 cp is enough to divert the acid to another interval with low permeability, 6% to 7% by volume concentration of VES solution has the that range of viscosity which is enough in acid diversion application as shown in fig. 1.

2.3 Temperature Effect on the Gelling Action

Reservoir temperature has an important impact on the performance of any injected chemicals into the reservoir, as temperature acts as a reaction rate accelerator. In our study we are

trying to understand the behavior of the VES under different temperature ranges to simulate the reservoir temperature effect. VES Solutions with different load concentrations 5, 6, 7, 8 & 10% of VES was examined to determine the limitations of VES application at different temperature ranges. In Fig (2) below shows that temperature has a negative impact on the VES gelling action behavior. At high temperature the VES loss its viscosity and break down to low viscosity solution. All curves in fig (2) show a peak value of viscosity at certain temperature, and then viscosity starts to decline with temperature increase which proves that temperature helps to a certain limit as a reaction rate accelerator to build up the viscosity of the VES solution then with higher temperature the viscosity starts to break down.

2.4 Visco-Elastic Behavior at Different Shear Rates

Visco-Elasticity is the ability of a gel to deform under stress and restore normal viscosity once the applied stress is removed. This feature is important in acid diversion mechanism as the pumped fluid exposure to different range of stresses through the formation; the pumping rate, tubing friction; drag force, formation permeability and friction inside the formations are aspects of the stress that gel exposed to. So to examine the Visco-Elastic capability of the selected VES is essential to understand the behavior of the VES within the formation. Different shear rates were applied on two different VES solutions 3% & 4% VES and then to observe the change of viscosity behavior at different shear rates. Moderate shear rate and very low shear rate were applied, to fully understand and assure the Visco-Elastic behavior of the subject surfactant VES over a wide range of shear rates. Fig (3) & (4) below show the VES viscosity responses to moderate and very low shear rates respectively.

2.5 Effect of Salts Concentration on VES Behavior

Formation water is full of salts such as NaCl& CaCl₂, once the VES solution is pumped to the formation it comes into contact with the formation water. Also, in acid diversion, the VES is carried by hydrochloric acid that reacts with the carbonate formations and release CaCl₂ as a reaction result. So, examine different concentrations of salts of on the VES behavior at different temperatures is important to understand the VES performance within the reservoir. Fig (5) shows a viscosity build-up with higher salt consternations, that result in a positive effect of the salts on the VES performance as higher viscosity is required to support the diversion action of the VES. Also fig (6) shows the temperature effect on VES solutions mixed with different concentrations of CaCl₂ salt. Temperature has a negative effect on the gel viscosity of the VES mixed with salts but the viscosity decline is not sharp and keeps the viscosity of the VES solution in the application range.

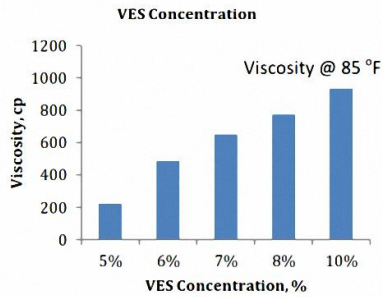


Fig.1. VES Concentration Effect.

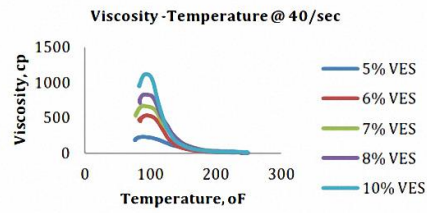


Fig. 2. Temperature Effect on VES.

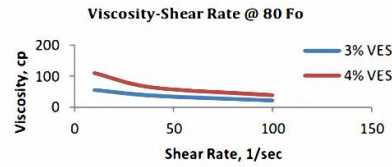


Fig. 3. Visco-Elastic Behavior of the VES.

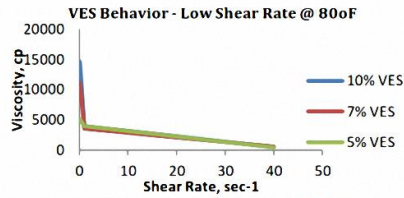


Fig. 4. Visco-Elastic Behavior of the VES.

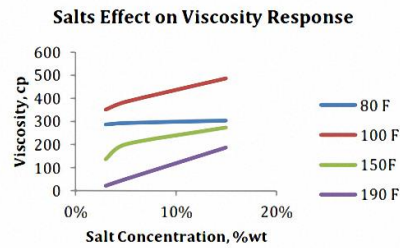


Fig. 5. Viscosity Response with Salts Concentration.

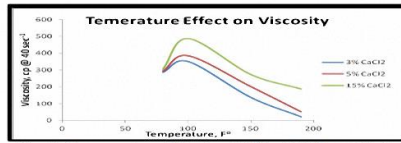


Fig. 6. Temperature Effect on VES at Different Salts Concentration.

3. Case Study

An oil well lies in the southern area of West Qurna field, Basra, Iraq, recently drilled into Mishrif carbonate formation at 2535m with a perforated interval of 100m. The reservoir average temperature is 177°F, and the oil is 32°API, no evidence for H₂S. The pay zone is of three intervals with different permeability and reservoir pressure as shown in fig (7), The well after completion was flowed back, showing very low productivity index, with a total daily production of 320 BOPD, the formation damage was attributed to the mud loss during the drilling of the pay zone, LCM (loss Circulating Material) was used to stop losses to the formation which includes medium calcium carbonate materials.

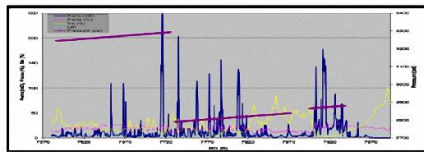


Fig. 7. Permeability Pressure of the Reservoir.

The decision was made to acid stimulate the pay zone to enhance the productivity and to create new channels to overcome the drilling and workover fluid damage. The perforated interval is 328 ft, and has permeability and pressure heterogeneity, so diversion in this case was important to have fair acid distribution. VES with 15% HCl acid diversion technique was selected due to its minimal residual damage compared to other chemical techniques. Table 1 shows the pumping schedule of the 15% HCl acid and the VES

acid diversion in stages, where fig (8) shows the pumping pressure changes due to the change in the pumped fluid and the effect of the gelling action. Change in pressure reflects the response of the formation resistance to the VES solution, pressure build-up was a result of the VES gelling action as the formed gels plugged the high permeable intervals and divert the acid the rest of the interval. The well then flowed back through coiled tubing nitrogen lifting, the well started to flow back and cleaning itself, once the spent acid out of the formation, the production has been diverted to the well test separator, the flowing period test showed a production of 2400 bbls/day @ 320psi WHP and 46” chock size.

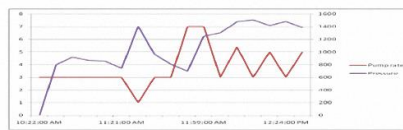


Fig. 8. Pressure Pumping Curve.

Table 1: Acid Treatment Pumping Schedule.

Pumping Procedure for Oil Production Well									
Buildup of 15% HCl With VES Diverter									
Time	Rate	Fluid	Pressure	Temp	Vis	Surf	Flow	Prod	Notes
0	0	Water	320	177	0.01	0	0	0	Initial
1	10	15% HCl	350	177	0.01	0	0	0	Start of acid
2	20	15% HCl	380	177	0.01	0	0	0	Pressure build-up
3	30	15% HCl	410	177	0.01	0	0	0	Pressure build-up
4	40	15% HCl	440	177	0.01	0	0	0	Pressure build-up
5	50	15% HCl	470	177	0.01	0	0	0	Pressure build-up
6	60	15% HCl	500	177	0.01	0	0	0	Pressure build-up
7	70	15% HCl	530	177	0.01	0	0	0	Pressure build-up
8	80	15% HCl	560	177	0.01	0	0	0	Pressure build-up
9	90	15% HCl	590	177	0.01	0	0	0	Pressure build-up
10	100	15% HCl	620	177	0.01	0	0	0	Pressure build-up
11	110	15% HCl	650	177	0.01	0	0	0	Pressure build-up
12	120	15% HCl	680	177	0.01	0	0	0	Pressure build-up
13	130	15% HCl	710	177	0.01	0	0	0	Pressure build-up
14	140	15% HCl	740	177	0.01	0	0	0	Pressure build-up
15	150	15% HCl	770	177	0.01	0	0	0	Pressure build-up
16	160	15% HCl	800	177	0.01	0	0	0	Pressure build-up
17	170	15% HCl	830	177	0.01	0	0	0	Pressure build-up
18	180	15% HCl	860	177	0.01	0	0	0	Pressure build-up
19	190	15% HCl	890	177	0.01	0	0	0	Pressure build-up
20	200	15% HCl	920	177	0.01	0	0	0	Pressure build-up
21	210	15% HCl	950	177	0.01	0	0	0	Pressure build-up
22	220	15% HCl	980	177	0.01	0	0	0	Pressure build-up
23	230	15% HCl	1010	177	0.01	0	0	0	Pressure build-up
24	240	15% HCl	1040	177	0.01	0	0	0	Pressure build-up
25	250	15% HCl	1070	177	0.01	0	0	0	Pressure build-up
26	260	15% HCl	1100	177	0.01	0	0	0	Pressure build-up
27	270	15% HCl	1130	177	0.01	0	0	0	Pressure build-up
28	280	15% HCl	1160	177	0.01	0	0	0	Pressure build-up
29	290	15% HCl	1190	177	0.01	0	0	0	Pressure build-up
30	300	15% HCl	1220	177	0.01	0	0	0	Pressure build-up
31	310	15% HCl	1250	177	0.01	0	0	0	Pressure build-up
32	320	15% HCl	1280	177	0.01	0	0	0	Pressure build-up
33	330	15% HCl	1310	177	0.01	0	0	0	Pressure build-up
34	340	15% HCl	1340	177	0.01	0	0	0	Pressure build-up
35	350	15% HCl	1370	177	0.01	0	0	0	Pressure build-up
36	360	15% HCl	1400	177	0.01	0	0	0	Pressure build-up
37	370	15% HCl	1430	177	0.01	0	0	0	Pressure build-up
38	380	15% HCl	1460	177	0.01	0	0	0	Pressure build-up
39	390	15% HCl	1490	177	0.01	0	0	0	Pressure build-up
40	400	15% HCl	1520	177	0.01	0	0	0	Pressure build-up
41	410	15% HCl	1550	177	0.01	0	0	0	Pressure build-up
42	420	15% HCl	1580	177	0.01	0	0	0	Pressure build-up
43	430	15% HCl	1610	177	0.01	0	0	0	Pressure build-up
44	440	15% HCl	1640	177	0.01	0	0	0	Pressure build-up
45	450	15% HCl	1670	177	0.01	0	0	0	Pressure build-up
46	460	15% HCl	1700	177	0.01	0	0	0	Pressure build-up
47	470	15% HCl	1730	177	0.01	0	0	0	Pressure build-up
48	480	15% HCl	1760	177	0.01	0	0	0	Pressure build-up
49	490	15% HCl	1790	177	0.01	0	0	0	Pressure build-up
50	500	15% HCl	1820	177	0.01	0	0	0	Pressure build-up
51	510	15% HCl	1850	177	0.01	0	0	0	Pressure build-up
52	520	15% HCl	1880	177	0.01	0	0	0	Pressure build-up
53	530	15% HCl	1910	177	0.01	0	0	0	Pressure build-up
54	540	15% HCl	1940	177	0.01	0	0	0	Pressure build-up
55	550	15% HCl	1970	177	0.01	0	0	0	Pressure build-up
56	560	15% HCl	2000	177	0.01	0	0	0	Pressure build-up
57	570	15% HCl	2030	177	0.01	0	0	0	Pressure build-up
58	580	15% HCl	2060	177	0.01	0	0	0	Pressure build-up
59	590	15% HCl	2090	177	0.01	0	0	0	Pressure build-up
60	600	15% HCl	2120	177	0.01	0	0	0	Pressure build-up
61	610	15% HCl	2150	177	0.01	0	0	0	Pressure build-up
62	620	15% HCl	2180	177	0.01	0	0	0	Pressure build-up
63	630	15% HCl	2210	177	0.01	0	0	0	Pressure build-up
64	640	15% HCl	2240	177	0.01	0	0	0	Pressure build-up
65	650	15% HCl	2270	177	0.01	0	0	0	Pressure build-up
66	660	15% HCl	2300	177	0.01	0	0	0	Pressure build-up
67	670	15% HCl	2330	177	0.01	0	0	0	Pressure build-up
68	680	15% HCl	2360	177	0.01	0	0	0	Pressure build-up
69	690	15% HCl	2390	177	0.01	0	0	0	Pressure build-up
70	700	15% HCl	2420	177	0.01	0	0	0	Pressure build-up
71	710	15% HCl	2450	177	0.01	0	0	0	Pressure build-up
72	720	15% HCl	2480	177	0.01	0	0	0	Pressure build-up
73	730	15% HCl	2510	177	0.01	0	0	0	Pressure build-up
74	740	15% HCl	2540	177	0.01	0	0	0	Pressure build-up
75	750	15% HCl	2570	177	0.01	0	0	0	Pressure build-up
76	760	15% HCl	2600	177	0.01	0	0	0	Pressure build-up
77	770	15% HCl	2630	177	0.01	0	0	0	Pressure build-up
78	780	15% HCl	2660	177	0.01	0	0	0	Pressure build-up
79	790	15% HCl	2690	177	0.01	0	0	0	Pressure build-up
80	800	15% HCl	2720	177	0.01	0	0	0	Pressure build-up
81	810	15% HCl	2750	177	0.01	0	0	0	Pressure build-up
82	820	15% HCl	2780	177	0.01	0	0	0	Pressure build-up
83	830	15% HCl	2810	177	0.01	0	0	0	Pressure build-up
84	840	15% HCl	2840	177	0.01	0	0	0	Pressure build-up
85	850	15% HCl	2870	177	0.01	0	0	0	Pressure build-up
86	860	15% HCl	2900	177	0.01	0	0	0	Pressure build-up
87	870	15% HCl	2930	177	0.01	0	0	0	Pressure build-up
88	880	15% HCl	2960	177	0.01	0	0	0	Pressure build-up
89	890	15% HCl	2990	177	0.01	0	0	0	Pressure build-up
90	900	15% HCl	3020	177	0.01	0	0	0	Pressure build-up
91	910	15% HCl	3050	177	0.01	0	0	0	Pressure build-up
92	920	15% HCl	3080	177	0.01	0	0	0	Pressure build-up
93	930	15% HCl	3110	177	0.01	0	0	0	Pressure build-up
94	940	15% HCl	3140	177	0.01	0	0	0	Pressure build-up
95	950	15% HCl	3170	177	0.01	0	0	0	Pressure build-up
96	960	15% HCl	3200	177	0.01	0	0	0	Pressure build-up
97	970	15% HCl	3230	177	0.01	0	0	0	Pressure build-up
98	980	15% HCl	3260	177	0.01	0	0	0	Pressure build-up
99	990	15% HCl	3290	177	0.01	0	0	0	Pressure build-up
100	1000	15% HCl	3320	177	0.01	0	0	0	Pressure build-up

4. Conclusions

- 1- The tested VES product is valid for oil field application at limited temperature range.
- 2- Concentration of the VES will depend on the purpose of the application. Higher concentrations of VES can build-up a solution with a viscosity of 1000 cp which can be used as a fluid loss control treatment.
- 3- Temperature affects negatively on the VES gelling action.
- 4- Salts support the viscosity build-up of the VES solution.
- 5- VES can successfully divert acid and allow fair acid distribution that will support enhancing the well productivity.

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References

1. **Tadros. T.T.** : Applied Surfactant: Principles and Applications, PP 19-26, First Edition, Wiley-VCH- USA, 2006.
2. **N. M. Os van, J. R. Hauk, L. A. M. Rupert.** : "Physic-chemical Properties of Selected Anionic, Cationic and Nonionic Surfactants", Elsevier, Amsterdam, 1993.
3. **E. H. Lucassen- Reynders:** "Anionic Surfactants – Physical Chemistry of Surfactant Action", Marcel Dekker, New York, 1981.
4. **Tadros. T.T.:** "Applied Surfactants: Principles and Applications" PP 113-125 Hoboken, Wiley-VCH, USA, 2006.
5. **S. S. Ashrawi.** "Hot water, surfactant, and polymer flooding process for heavy oil". Patent: US 5083612, 1992.
6. **N.H. Ginest,:** "Field Evaluation of Acid simulation Divorter Materials and Placement Methods in Arab-D Injection Wells with Open hole Completion", paper SPE 25412 presented at the 1993 Middle East Oil Technical Conference and Exhibition, Bahrain, 3–6, April 1993.
7. **S.J. Black , and J.L Rike,:** "The Role of the Consultant in Meeting the Formation Damage Challenge," paper SPE 5700, presented at the SPE Symposium on Formation Damage Control, Houston, Texas, USA (January 29–30, 1976).
8. **A. Joseph, E Leon, and M. Scott, SPE,:** "Characterization and Evaluation of Formation Damage During Water Flooding of A High Clay Content Reservoir" Paper SPE 16234 MS, Reservoir Engineering, Nov. 1988.
9. **J. MaGee, M.A., and R. Pongratz,:** "Method for Effective Fluid Diversion when Performing a Matrix Acid Stimulation in Carbonate Formations," paper SPE 37736 presented at the 1997 Middle East Oil Show, Bahrain, 15-18 March 1997.
10. **A.Toseef and D.J. Beaman, SPE, Halliburton, and P. Birou, Total E&P.:** "Viscoelastic Surfactant Diversion: An Effective Way to Acidize Low-Temperature Wells" Paper SPE 136574-MS, Abu Dhabi International Petroleum Exhibition and Conference, 1-4 November 2010, Abu Dhabi, UAE.