

SIMULTANEOUS CONDENSATION-EVAPORATION HEAT TRANSFER ON A VERTICAL TUBE, I- EXPERIMENTAL STUDY

انتقال الحرارة بالتكثيف والتبخير الآنيين من أنبوب رأسي I -دراسة معملية

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خلاصة

هذا البحث يقدم دراسة معملية لانتقال الحرارة بالتكثيف والتبخير الآنيين من أنبوب رأسي. وقد تم تصميم وتنفيذ دائرة اختبار معملية يتم خلالها تكثيف بخار الماء على السطح الخارجى للأنبوب الرأسي تاركا الحرارة الموجودة به للماء المراد تبخيره والذي يتساقط من أعلى إلى أسفل كطبقة رقيقة على السطح للدخلى للأنبوب فيكتسب هذه الحرارة ويتم تبخير جزء من هذا الماء. وقد تم قياس درجات الحرارة والضغط والتدفق لكل من المسائين وذلك لمعالجتها وتحليلها لحساب معامل انتقال الحرارة ورقم نوسلت لكل من التكثيف والتبخير كل على حده ولهما معا عند ظروف تشغيل مختلفة. أجريت لتجارب عند قيم مختلفة لمعدل سريان الماء ودرجة حرارة دخوله وكذلك لمعدل سريان بخار ماء الجاف المشبع وضغطه.

وقد أظهرت النتائج أن معامل انتقال الحرارة ورقم نوسلت يزيدان مع نقصان رقم رينولدز للماء المتساقط. وقد تم استنتاج صيغة رياضية لرقم نوسلت لعملية التكثيف - للتبخير كدالة في عوامل التشغيل التي تمت دراستها في هذا البحث.

ABSTRACT

In the present work, simultaneous condensation-evaporation heat transfer in thin films on a vertical tube is, experimentally, investigated. Condensation takes place on the outer surface of the vertical tube and the evaporation occurs inside it. The condensed steam outside the tested tube imparts its latent heat to evaporate the thin liquid film, which flows inside the tube. Throughout this work, the range of Reynolds number for water film flow is from 50 to 800, while that of condensate outside the tube, takes values less than 100.

The studied operating parameters, which affect the condensation-evaporation processes are water flow rate, its degree of subcool, the flow rate of the dry saturated heating steam and its pressure. The flow rate of the falling heated water is 3-50 kg/hr at constant pressure of 1.1 bar, while the heating steam flow rate is up to 5 kg/hr at a pressure which varies from 1.2 to 2 bar.

The results show that, decreasing the Reynolds number of the falling water film, up to dry out at the end of the vertical tube, causes an increase of heat transfer coefficient for different operating parameters. In addition, the Nusselt number for different values of Reynolds number are calculated and in accordance, an empirical correlation for the condensation - evaporation Nusselt number as a function of the studied operating parameters is proposed.

Key words: Condensation - Evaporation - Vertical tube

NOMENCLATURE

A	Surface area	m^2
c_p	Specific heat at constant pressure	$J/kg \cdot K$
d_m	Mean diameter of the tube	m
h	Heat transfer coefficient	$W/m^2 \cdot K$
h_{fg}	Latent heat	J/kg

k	Thermal conductivity	$W/m \cdot K$
L	Vertical tube height	m
m	Mass flow rate	kg/s
Nu	Nusselt number	--
p	Pressure	Pa
Pr	Prandtl number	--
Q	Heat transfer rate	W
q''	Heat flux	W/m^2
Re	Reynolds number	--
R_o	Ratio between Reynolds number for heating steam and Reynolds number for heated water film	--
T	Temperature	$^{\circ}C$
U	Condensation – evaporation heat transfer coefficient	$W/m^2 \cdot K$
Greek symbols		
μ	Dynamic viscosity of heated water-film	$kg/m \cdot s$
Subscripts		
av	Average	
c	Condensation	
$c-e$	Condensation-evaporation	
e	Evaporation	
i	Inlet	
l	Lost	
o	Outlet	
sat	Saturated	
sub	Degree of subcool	
w	Wall	

1. INTRODUCTION

The phenomenon of film condensation-evaporation occurs in many practical situations and is of great interest in several technical areas specially heat exchange devices such as desalination units, heat exchangers, refrigeration units, petroleum refinery and food industries ...etc. Yan et al [1-2] studied, experimentally and numerically, the evaporative cooling of liquid film in vertical channel. A numerical analysis was carried out to study the detailed heat transfer characteristics of a falling liquid film by solving the governing equations for the liquid film and induced gas flow together. The measured data were in good agreement with the numerical prediction.

Condensation over surfaces was studied in considerable detail [3-5]. Legay et al [3] studied, experimentally and numerically, heat transfer in an incompressible boundary layer associated with condensation over a vertical flat plate. Condensation effects may be used in various problems, to improve the efficiency of some heat exchangers. Experimental and numerical calculations were performed for laminar boundary layer. Experimental study of the interface between a condensing vapor region and an interfacing fluid was carried out by Jaluria [4]. The study considered the steady state and transient behavior of the interface. Forced convective film condensation inside vertical tube was performed by Chen et al [5].

Simultaneous condensation-evaporation process, at different values of operating conditions, was analyzed by Mahgoub et al [6]. The effects of heat flux, falling mass flow rate and pressure ratio on local and average heat transfer coefficients are investigated, experimentally and theoretically, for horizontal tube. Empirical correlation relating the dimensionless groups, which govern the evaporation and condensation in laminar flow region, was proposed. Moalem et al [7] and Sideman et al [8] studied overall heat transfer coefficient in horizontal evaporator-condenser tube in case of low heat flux and laminar flow regime.

Seeking for good understanding of simultaneous evaporation-condensation process, more studies are needed to be carried out. In the present work, heat transfer by simultaneous condensation- evaporation process on vertical tube wall is, experimentally, studied.

2. EXPERIMENTAL TEST-RIG

To study the simultaneous condensation-evaporation process on a vertical tube, a test-rig is designed and constructed, such that the condensation takes place at the outer surface of the tested tube; while the evaporation occurs at its inner surface. The layout of the test-rig is illustrated in figure (1-a). It consists of two loops, the first one is associated with the heating steam, while the second loop is for the heated inner water-film.

Considering the heating steam loop, the generated steam is produced using a boiler of 9 kW rated power (2) and of 0.4-m diameter and 0.6-m height. To insure that, the heating steam enters the test section (1) dry and saturated, it passes through a water trap (3). The heating steam imparts its latent heat to the heated inner water-film, as it flows along the outer surface of the tested tube and it, consequently, becomes liquid water at the bottom of the test section. This condensed steam is directed to the boiler and there it is re-boiled.

On the other hand, considering the loop of the heated water-film, the water is led; from a constant water-level tank (5), to a stainless steel tested tube of 19-mm diameter, thickness 1mm and 1-m height. As the heated water flows along the inner surface of the tested tube, some of the water is evaporated. This evaporated water is directed to condenser (4), while the rest of the heated water is directed to the boiler (2).

Figure (1-b) shows the details of the test section. The heated water enters the test tube (1) through the adjustable position (guide) plate (2). This guide plate is mounted at the inlet of the test tube, to control the mass flow rate of heated water. Another job of it is to insure that the water flows along the tube as a thin liquid film adjacent to the inner surface of the tested tube (1). Heating steam enters the test section through the port (8) and leaves it, a condensate, through the port (4). To insure that, the heating steam condenses, only, at the outer surface of the tested tube (1), an insulating steam jacket (7) is used. The steam used in this jacket is of the same condition of the heating steam of the tested tube (inlet from port (11) and exit from port (12)).

Pressure and temperature of both heating steam and heated water are measured at their corresponding inlet cross-sections using Bourdon tube dial gauge and K type thermocouples; respectively. The temperature of condensate (of the heating steam) is, also, measured at its exit (at the bottom of the test section). The flow rate of the heating steam and the evaporated vapor, as liquid water, is measured by calibrated tank. The temperature of the outer surface of the tested tube is measured at three positions along the tube length.

3. DATA REDUCTION

The measured temperature, pressure and mass flow rate of both heating steam and heated water-film are used to calculate condensation, evaporation and condensation-evaporation heat transfer coefficients and, in turn, the corresponding Nusselt number. The imparted heat from the heating steam can be estimated according to the following relation as:

$$Q_c = m_c \cdot [h_{fg,c} + c_p(T_{sat,c} - T_{c,o})] \quad (1)$$

Where m_c , $h_{fg,c}$, c_p , $T_{sat,c}$ and $T_{c,o}$ are mass flow rate of heating steam, latent heat of condensation, specific heat at constant pressure, saturation temperature of heating steam and the temperature of the leaving condensed steam; respectively. The amount of heat transferred to the evaporated water film is:

$$Q_e = m_e \cdot [h_{fg,e} + c_p(T_{sat,e} - T_{e,i})] \quad (2)$$

Where m_e , $h_{fg,e}$, c_p , $T_{sat,e}$ and $T_{e,i}$ are mass flow rate of evaporated vapor, latent heat of evaporation, specific heat at constant pressure, saturation temperature of evaporated vapor and the temperature of the water-film at the inlet cross-section; respectively. The heat transferred to the un-evaporated part of the water-film is estimated as the difference between the heat transferred from the heating steam; equation (1) and that transferred to the evaporated part of water film; equation (2). This quantity of heat can be estimated according to the following equation:

$$Q_l = Q_c - Q_e \quad (3)$$

Q_l may be considered as the lost heat through the evaporation process. One can neglect the heat loss compared to the heat of heating steam. The heat flux can be defined according to the following relation as:

$$q'' = Q_c / A \quad (4)$$

Where A is the heat transfer surface area, which is defined as; $A = \pi d_m L$. The mean diameter of the tested tube and the tube height are denoted by d_m and L ; respectively.

Condensation, evaporation and condensation-evaporation heat transfer coefficients are defined according to the following equation:

$$h_c = q'' / (\Delta T)_c, \quad h_e = q'' / (\Delta T)_e \quad \& \quad U = q'' / (\Delta T)_{c-e} \quad (5)$$

Where h_c , h_e and U are heat transfer coefficient of condensation side, evaporation side and condensation - evaporation; respectively. $(\Delta T)_{c-e} (= T_{sat,c} - T_{sat,e})$; is the total temperature difference, while $(\Delta T)_c (= T_{sat,c} - T_{w,c})$ denotes the temperature difference in condensation side and $(\Delta T)_e$ is the temperature difference in the evaporation side $[(\Delta T)_e = T_{w,e} - T_{sat,e}]$. The wall temperature at the condensation and evaporation sides are denoted by $T_{w,c}$ and $T_{w,e}$; respectively. In accordance, one can define the corresponding Nusselt number for the condensation, evaporation and condensation-evaporation as:

$$Nu_c = h_c \cdot d_m / k, \quad Nu_e = h_e \cdot d_m / k \quad \& \quad Nu_{c-e} = U \cdot d_m / k \quad (6)$$

Where k is the thermal conductivity of the corresponding film and at its average temperature. Through out the present work, the Reynolds number has the following definition:

$$Re = m_c / \pi d \mu \quad (7)$$

Where μ is the dynamic viscosity of the heated water-film.

The uncertainties are determined for both measured and calculated quantities. The uncertainty of temperature difference is estimated as about 0.142 °C, while the largest calculated uncertainties in the Reynolds number was found to be about 3.1 % and that of Nusselt number is about 12.6%.

4. RESULTS AND DISCUSSIONS

Figure (2) shows the relation between the heat flux and the saturation temperature difference, between the condensation and evaporation sides for all studied cases, at different operating conditions. Throughout the present study, the degree of subcool for the falling water film is in the range 2-30 °C. During the experiments, the condensate leaves the tube, almost, as saturated water.

The evaporated vapor mass flow rate versus mass flow rate of heating steam, for the whole range of the studied operating conditions, is presented in figure (3). It is generally observed that, the evaporated vapor flow rate is less than the heating steam mass flow rate by a slight value. However, for some operating conditions the falling water-film, of higher values of degree of subcool, consumes a considerable amount of heat, in such a case, a decrease of the amount of evaporated vapor is expected.

The Nusselt number and heat transfer coefficients of condensation and evaporation against Reynolds number are shown in figure (4) at the heating steam pressure of 1.6 bar and heat flux of 22 kW/m². It is observed that, condensation heat transfer coefficient is greater than evaporation heat transfer coefficient for all carried out experiments. In addition, both condensation and evaporation heat transfer coefficients increase with decreasing Reynolds number. Nusselt number has the same behavior like that of heat transfer coefficient for both condensation and evaporation.

The Nusselt number ($Nu_{c,e}$) and heat transfer coefficient (U) of simultaneous condensation-evaporation process versus Reynolds number of the heated water-film (Re) are illustrated in figure (5). It is observed that for all values of Reynolds number, that the Nusselt number takes higher values for higher heat flux. At certain heat flux, Nusselt number increases with decreasing Reynolds number. This increase in Nusselt number (and heat transfer coefficient) can be explained as, the decrease in Reynolds number causes a decrease in the water-film thickness and, in turn, the thermal resistance decreases.

The experimental results in the considered range of Reynolds number (50-800) shows that, the average Nusselt number may be related to Reynolds number by the following proposed correlation:

$$Nu_{c,e} = 16.94 Re^{0.3} R_o^{1.6} Pr^{2.8} \quad \text{for } 1.5 < Pr < 2.25 \quad (8)$$

Where R_o ($R_o = Re_c / Re_e$) is the ratio between Reynolds number of heating steam, and that of the heated water-film.

The effect of saturation temperature difference (ΔT_{sat}) on the condensation – evaporation Nusselt number is shown in figure (6). The increase of this temperature difference causes an expected decrease in the heat transfer coefficient and consequently in Nusselt number for the same value of heat flux. As it is clear from the same figure, decreasing degree of subcool increases Nusselt number and heat transfer coefficient, for the same value of Reynolds number. Referring to the definition of Reynolds number [equation (7)], one can see that, this increase of both Nusselt number and heat transfer coefficient may be due to the decrease of the water-film thickness.

A comparison between the present results and that of other previous works in [7] is shown in figure (7). The present proposed correlation as represents fairly good, the actual present results is shown in figure. Although the values of the case vertical tube are higher than that of [7], the obtained Nusselt number of condensation- evaporation for horizontal tube after [7] has the same trend as that of present results. There is no data available in both condensations –evaporation in vertical tube but the previous work has the condensation only or evaporation only in vertical tube.

CONCLUSIONS

In the present work, simultaneous condensation-evaporation heat transfer on a vertical tube was, experimentally, studied at different operating parameters. Condensation takes place on the outer surface of the vertical tube and evaporation on it inside surface. The studied operating parameters are flow rate and degree of subcool of heated water-film, and flow rate of dry saturated heating steam and its pressure.

The results show that, condensation-evaporation Nusselt number increases with increasing heat flux. In addition, Nusselt number of condensation and evaporation, and Nusselt number for simultaneous condensation-evaporation are increased with decreasing Reynolds number. A correlation for Nusselt number as a function of the flow parameters is proposed.

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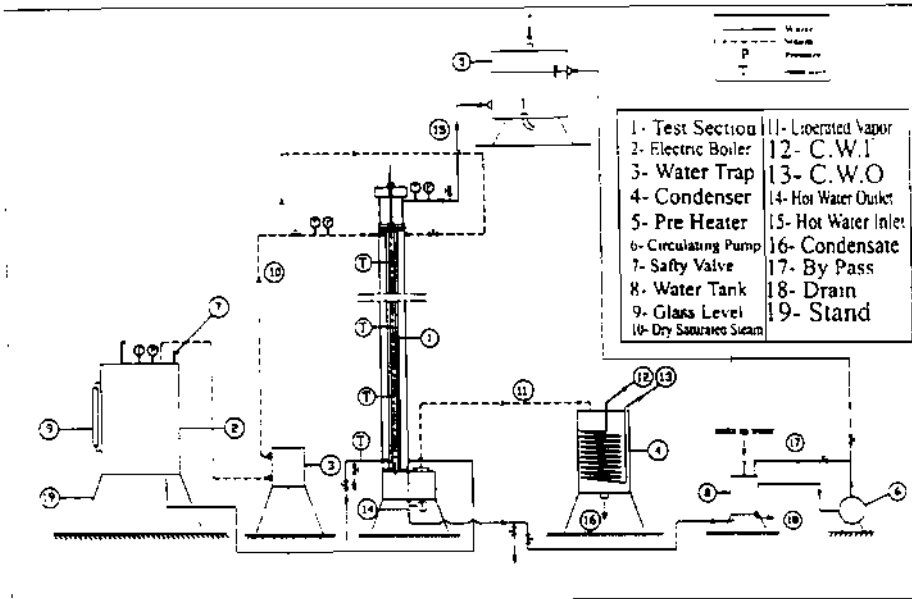


Fig.(1.a) Schematic layout of test -rig

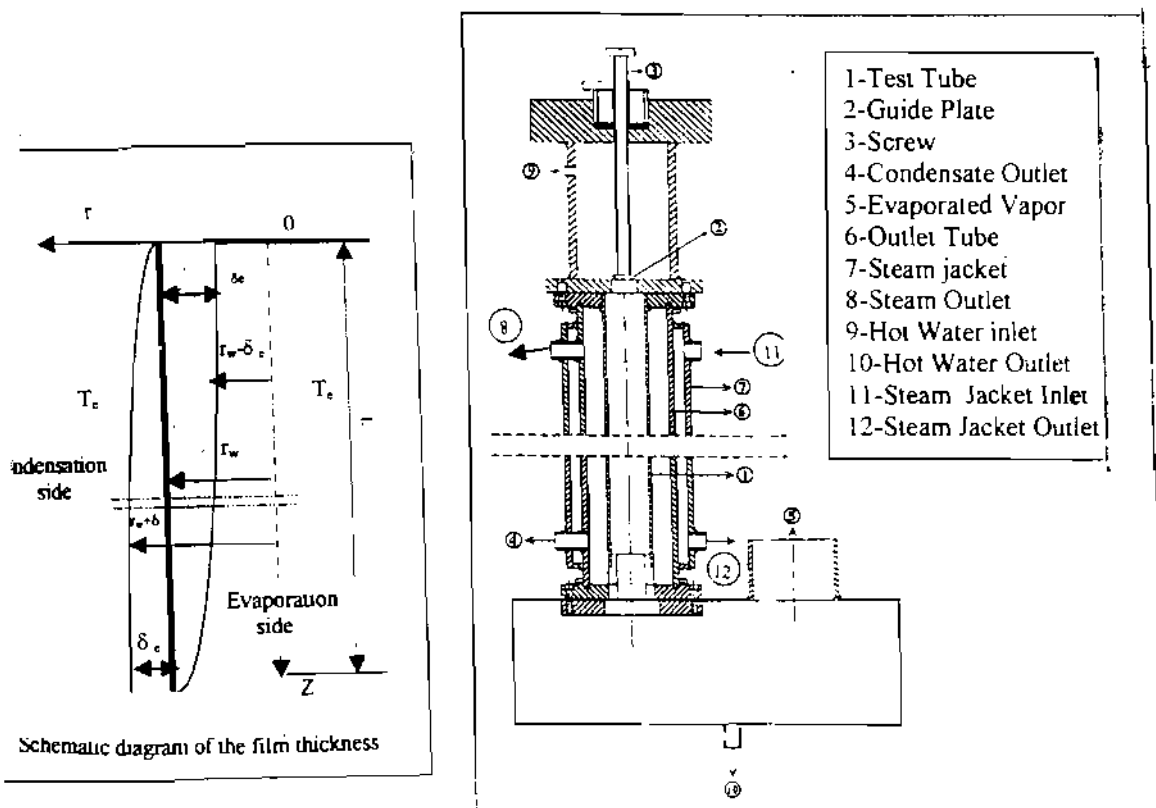


Fig (1.b) Test section

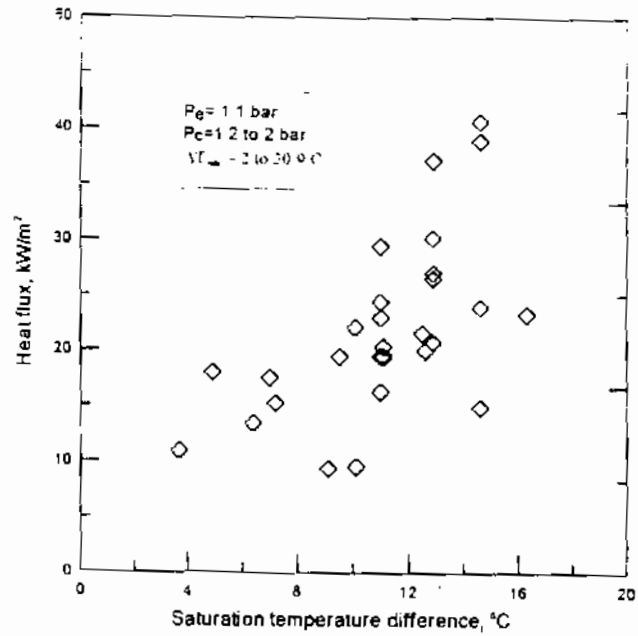


Fig. (2) Heat flux versus saturation temperature difference between condensation and evaporation sides for the whole range of the studied operating conditions

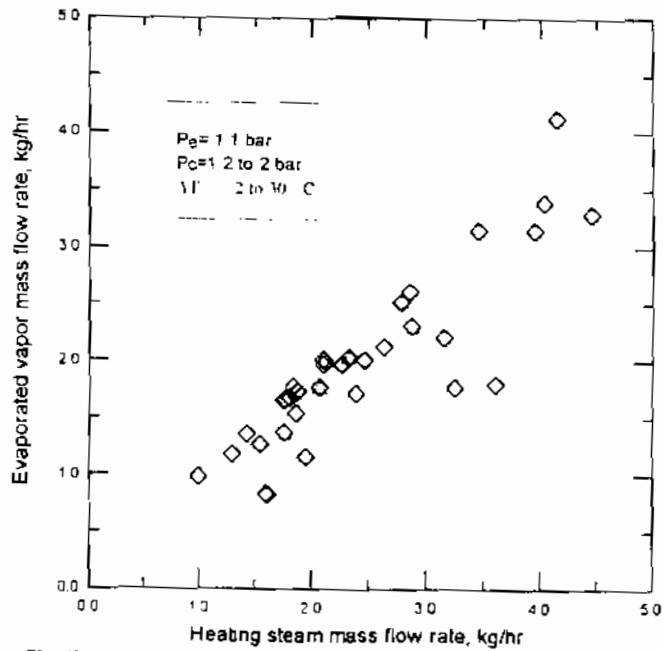


Fig. (3) Evaporated mass flow rate versus heating steam mass flow rate for the whole range of the studied operating conditions

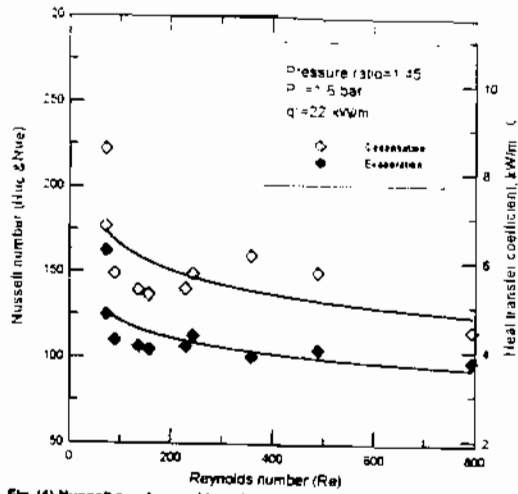


Fig. (4) Nusselt number and heat transfer coefficient for condensation and evaporation sides versus Reynolds number

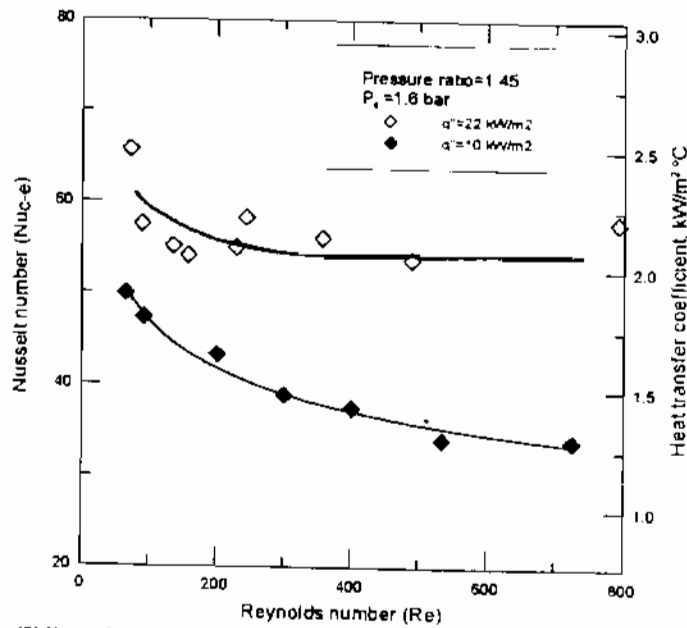


Fig. (5) Nusselt number and heat transfer coefficient versus Reynolds number for simultaneous condensation-evaporation process

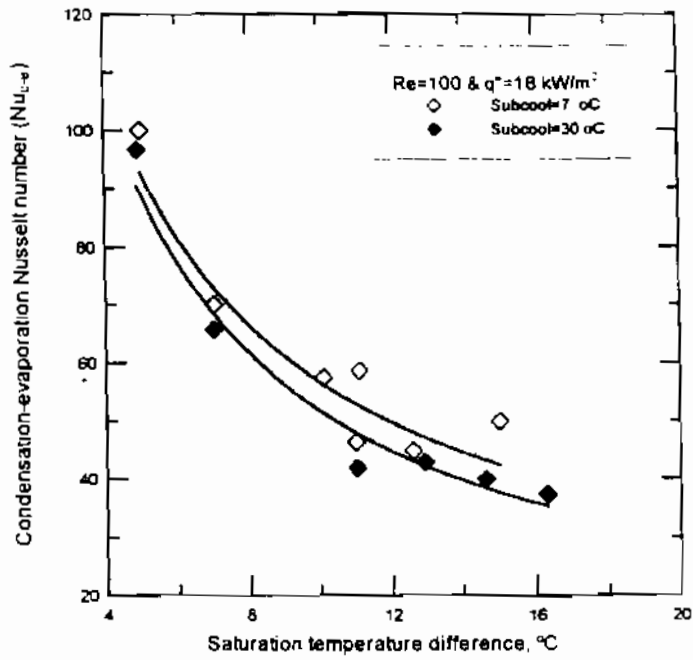


Fig. (6) Nusselt number versus saturation temperature difference for different degree of subcool

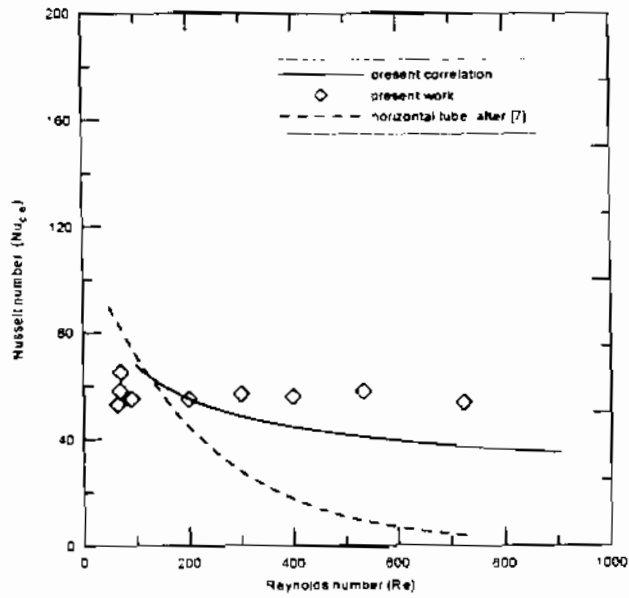


Fig. (7) Comparison between the present work and previous work